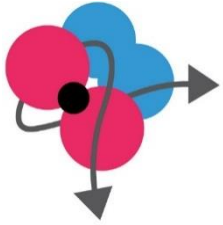
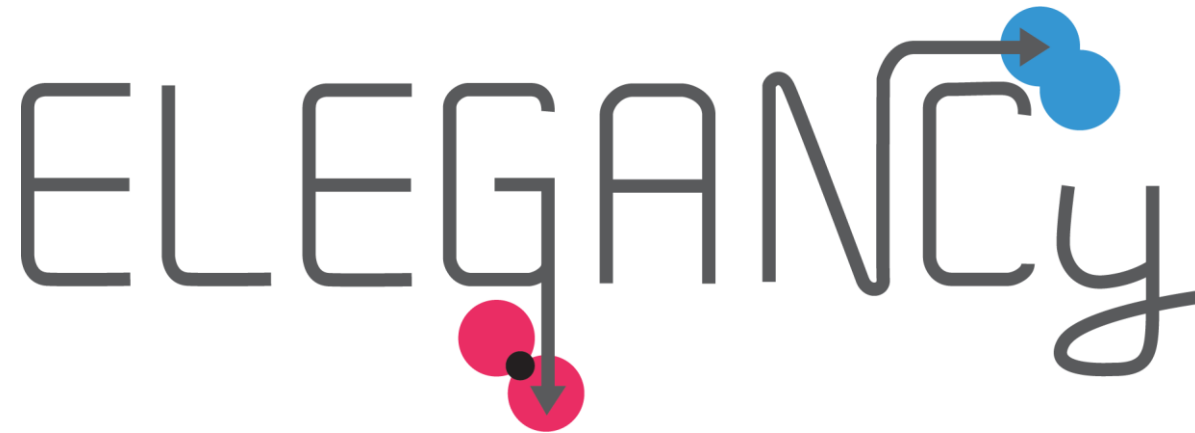


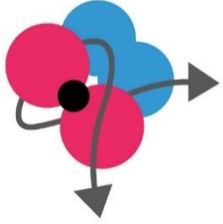
# ELEGANCy



## Towards an Accurate and Consistent Description of Thermodynamic Properties of Mixtures of CO<sub>2</sub> with Brines

Roland Span and Benedikt Semrau

WEBINAR 3: HYDROGEN SUPPLY AND CO<sub>2</sub> INJECTION AND STORAGE



# Empirical Helmholtz Energy Based Mixture Models

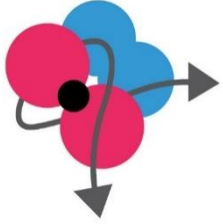
- Mixtures are described based on the 1990's approach by Lemmon & Tillner-Roth
  - Pure fluid equations of state
  - Mixing rules for  $\delta_m$  und  $\tau_m$  with up to 4 adjustable parameters
  - “Departure function” for an improved description of well measured mixtures

$$\alpha(\delta, \tau, \bar{x}) = \sum_{i=1}^N x_i \left[ \alpha_{oi}^0(\rho, T) + \ln x_i \right] + \sum_{i=1}^N x_i \alpha_{oi}^r(\delta_m, \tau_m) + \sum_{i=1}^{N-1} \sum_{j=i+1}^N x_i x_j F_{ij} \alpha_{ij}^r(\delta_m, \tau_m)$$

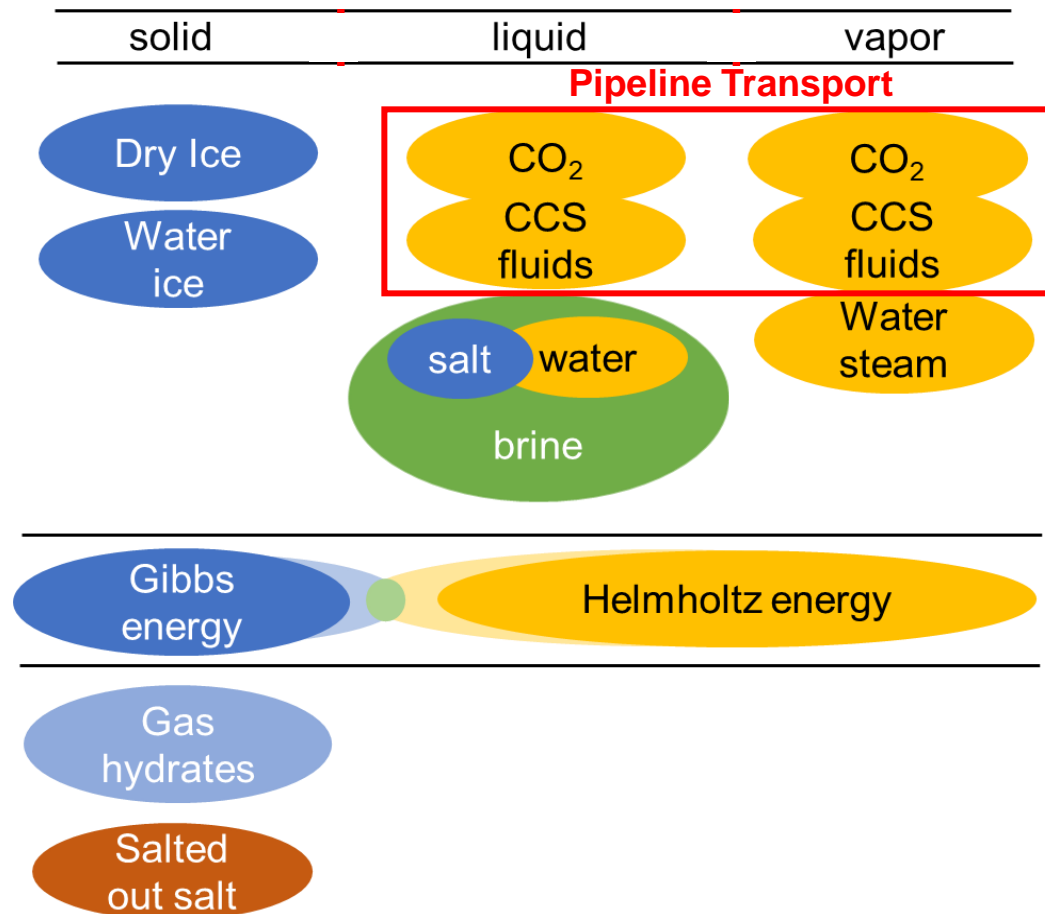
corresponding states  
with four parameters

departure function

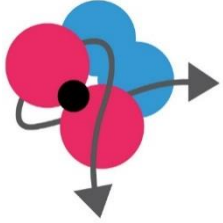
- **In multicomponent mixtures models for all binary subsystems required**
- **Four Levels of accuracy:** (a) purely predictive description with combination rules, (b) fitting of the four corresponding states parameters, (c) generalized departure function, (d) binary specific departure function



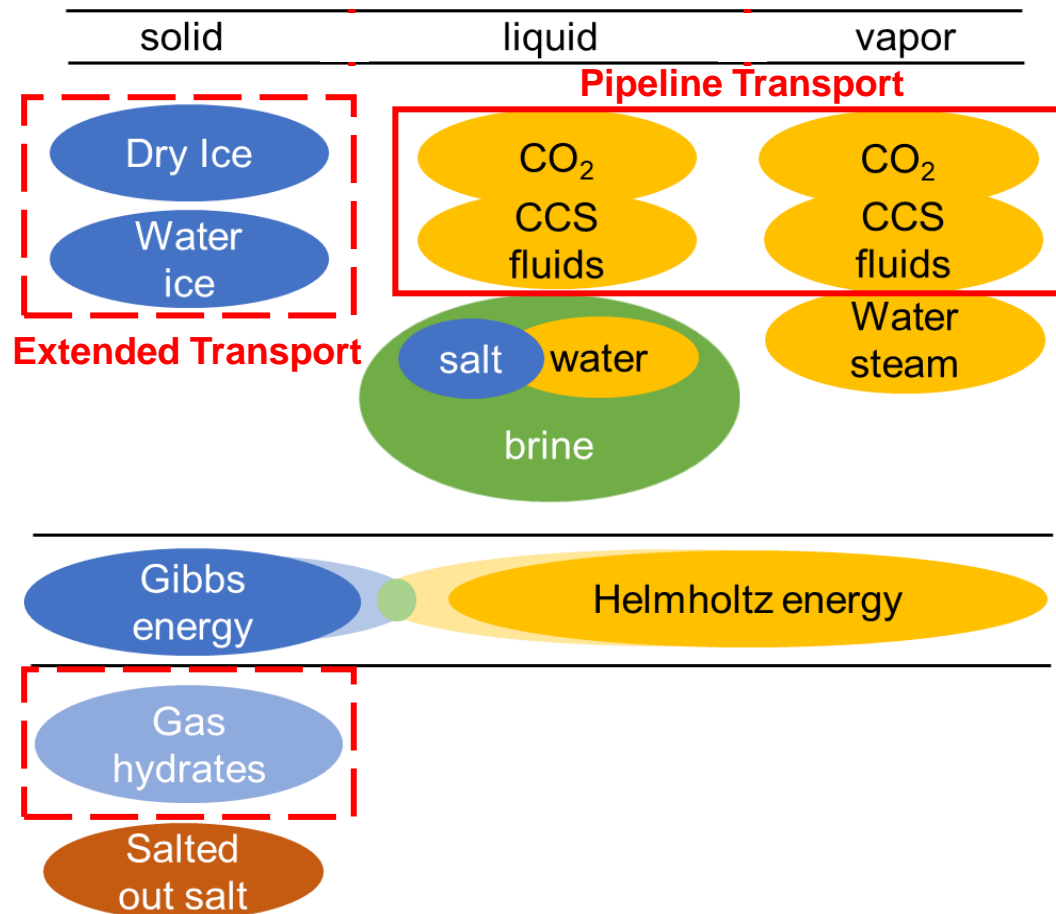
# Phases to be Considered in ELEGANCY



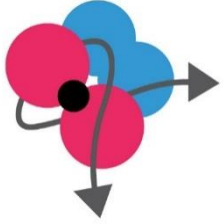
- Different phases are formulated in different types of fundamental equations
- Link between these property models is important for consistent models and calculations



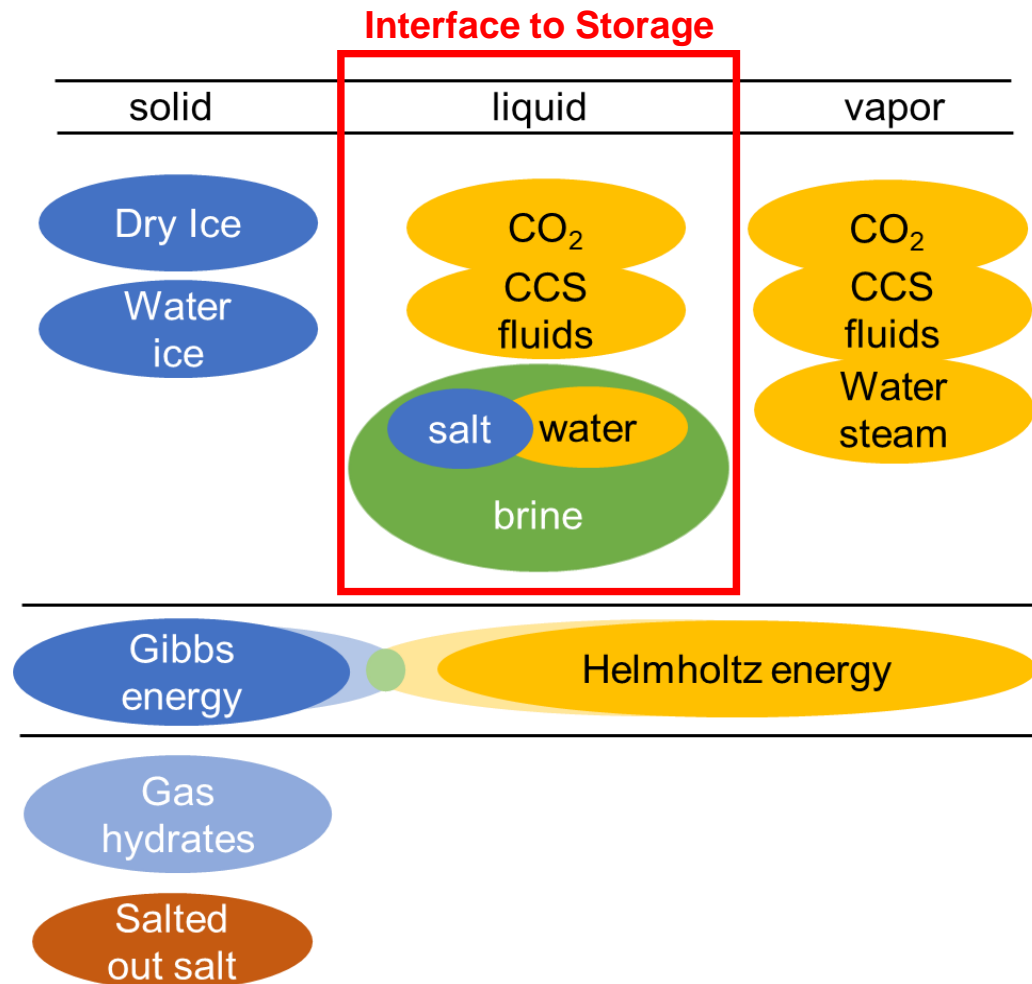
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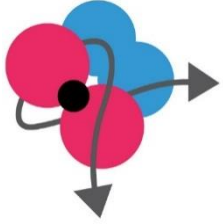
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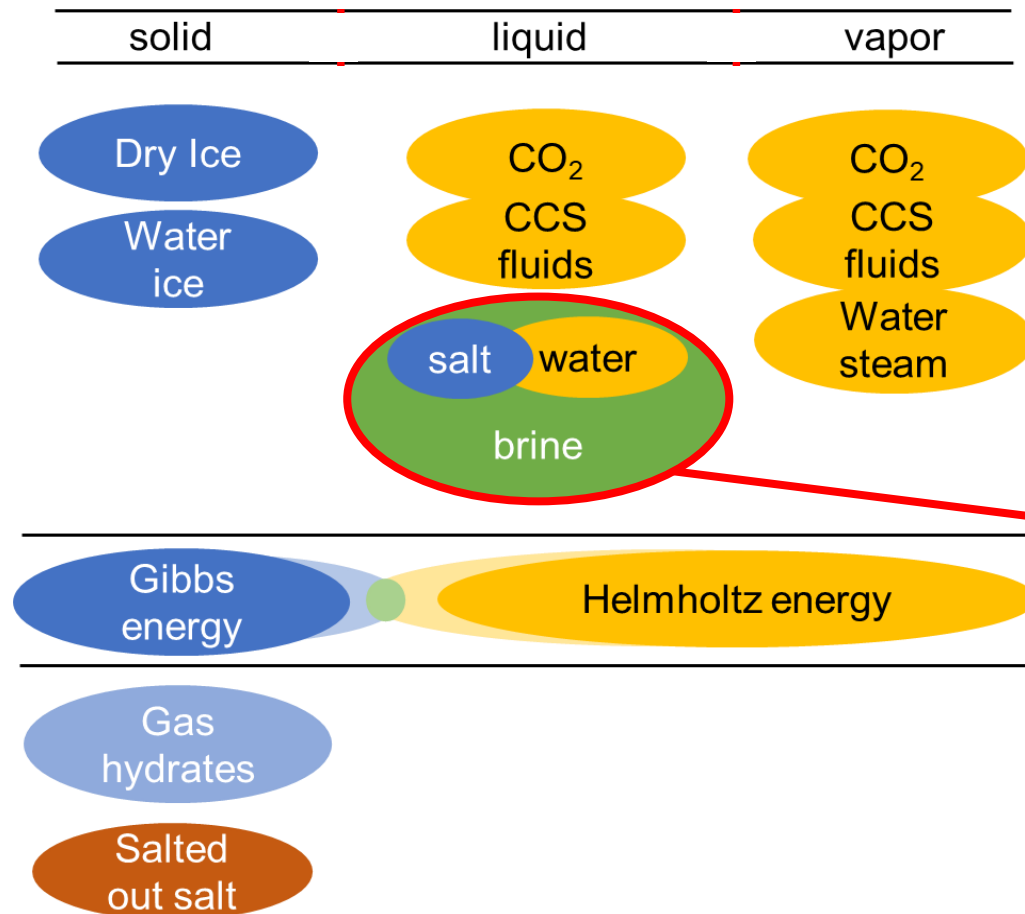
# Phases to be Considered in ELEGANCY



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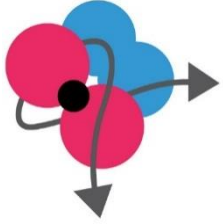


# Phases to be Considered in ELEGANCY



- Different phases are formulated in different types of fundamental equations
- Link between these property models is important for consistent models and calculations

**1<sup>st</sup> approach / feasibility check:** use the Gibbs energy based seawater equation of state by IAPWS to describe saltwater as liquid phase (IAPWS / IAPSO standard IAPWS R13-08 from 2008)



# Combining EOS in Helmholtz and Gibbs Energy

- Both EOS are fundamental equations of state but are formulated in different potentials that have different independent variables
- Helmholtz and Gibbs energy and their independent variables can be transferred via Legendre transformation
- Equality of properties allows for the determination of equivalent derivatives

$$p(T, \rho) = [1 + \delta \alpha_{\delta}^r] \rho RT$$

$$\delta \alpha_{\delta}^r = \frac{p}{\rho RT} - 1$$

$$\frac{1}{\rho} = \frac{\partial g(T, p)}{\partial p} = g_p$$

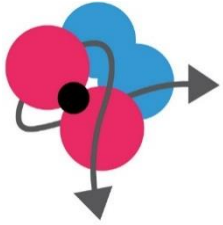
$$\delta \alpha_{\delta}^r = \frac{p g_p}{RT} - 1$$

$$\delta = \rho / \rho_c$$

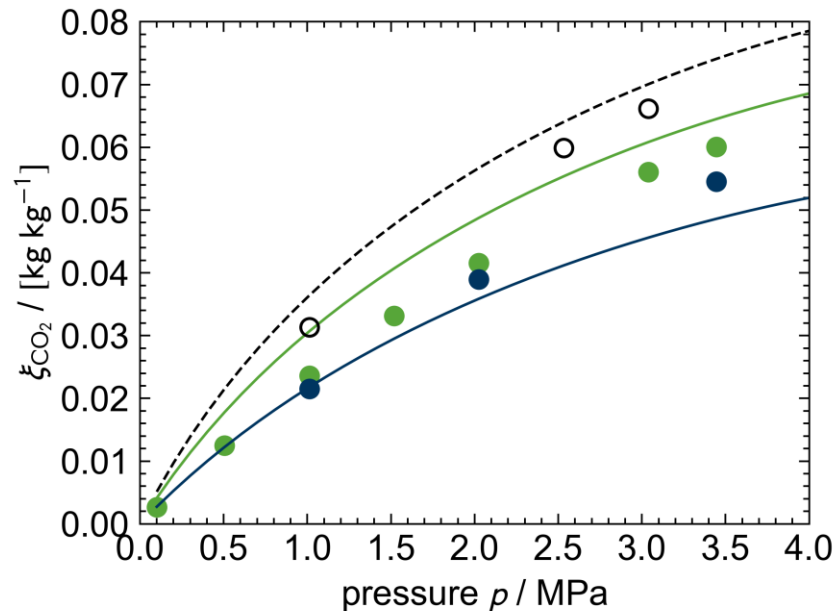
$$\alpha = a(T, \rho) / (RT) = \alpha^0 + \alpha^r$$

$$\alpha_{\delta}^r = (\partial \alpha^r / \partial \delta)_{\tau}$$

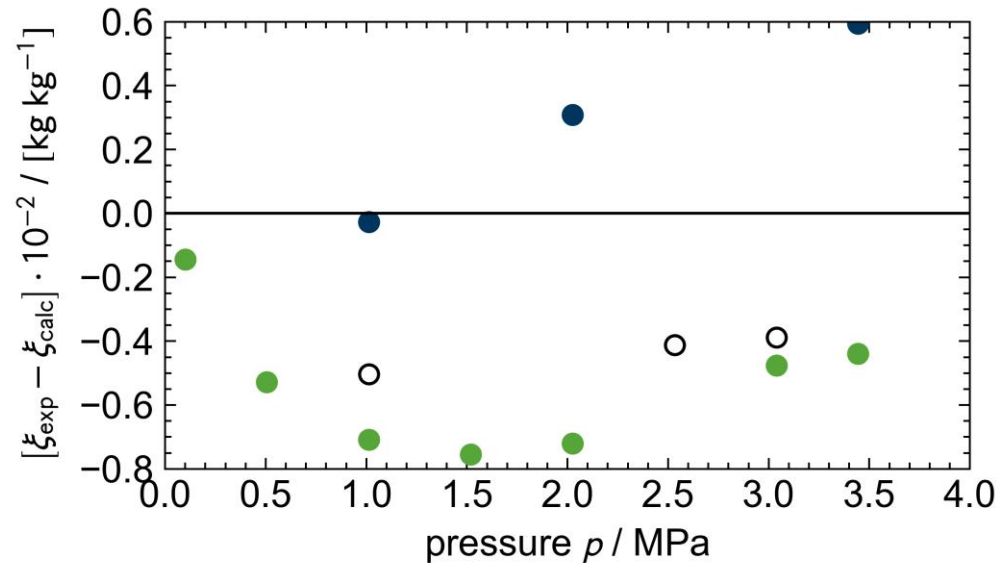
$$g_p = (\partial g / \partial p)_{T}$$



# Test Case: Solubility Data for CO<sub>2</sub> in Seawater

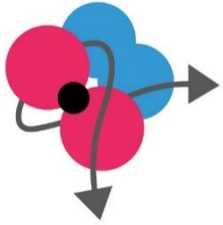


- Stewart & Munjal  $S_A = 0.0966 \text{ kg kg}^{-1}$
- Stewart & Munjal H<sub>2</sub>O+CO<sub>2</sub>
- Stewart & Munjal  $S_A = 0.0344 \text{ kg kg}^{-1}$
- EOS-CG 2016, H<sub>2</sub>O+CO<sub>2</sub>
- This model,  $S_A = 0.0344 \text{ kg kg}^{-1}$
- This model,  $S_A = 0.0966 \text{ kg kg}^{-1}$

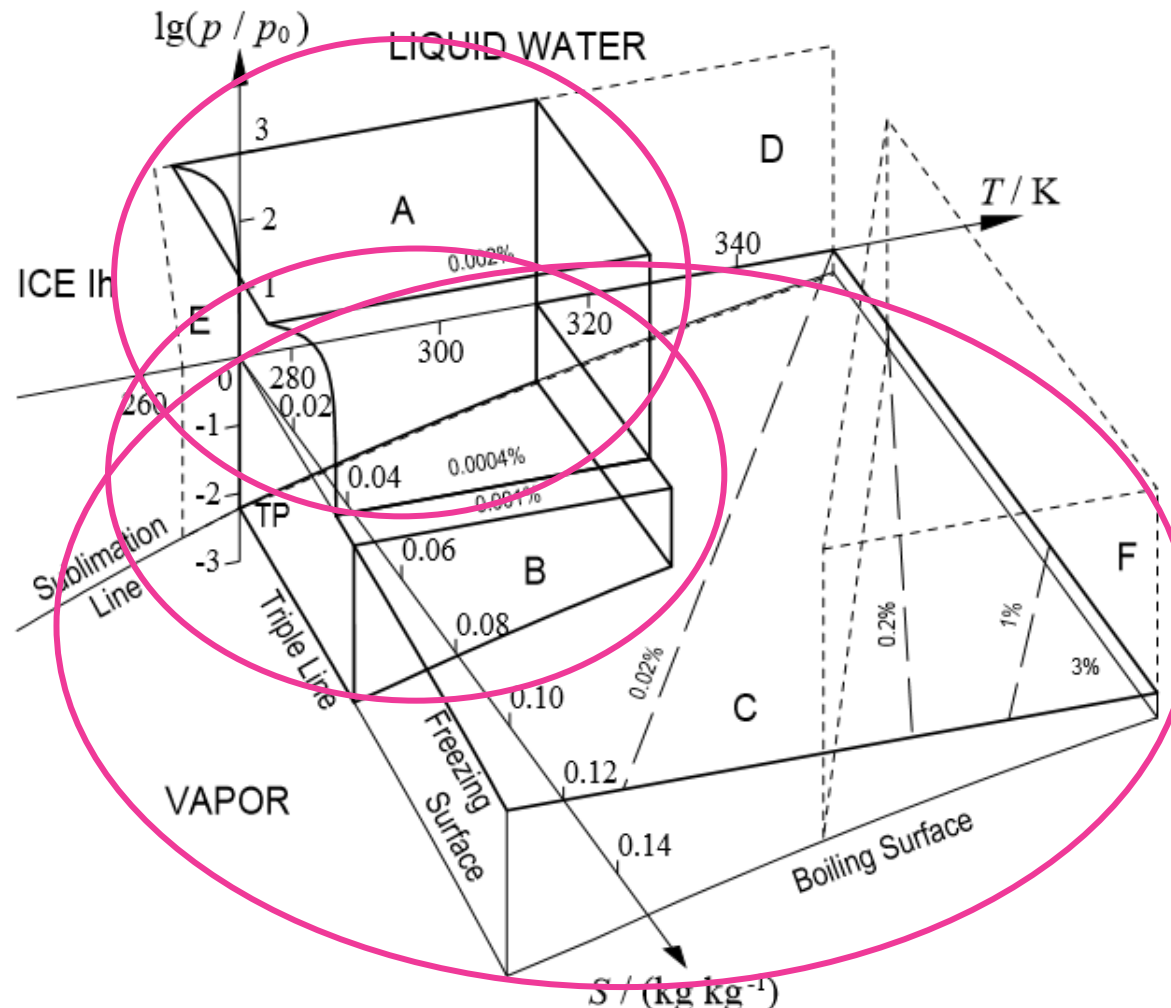


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# Range of Validity and Limitations



- $0 \leq S_A \leq 0.12 \frac{\text{kg}}{\text{kg}}$
- $261 \text{ K} \leq T \leq 353 \text{ K}$
- $0 < p \leq 10^8 \text{ Pa}$

Overall area,  
limitations below

- $0 \leq S_A \leq 0.042 \frac{\text{kg}}{\text{kg}}$
- $T_F \leq T \leq 313 \text{ K}$
- $101325 \text{ Pa} < p \leq 10^8 \text{ Pa}$

„Neptunian range“ (A)

- $0 \leq S_A \leq 0.05 \frac{\text{kg}}{\text{kg}}$
- $T_F \leq T \leq 313 \text{ K}$
- $p_{\text{vap}} < p \leq 101325 \text{ Pa}$

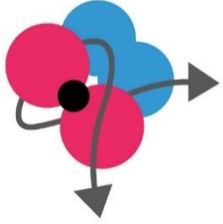
„low-pressure range“ (B)

- $0 \leq S_A \leq 0.12 \frac{\text{kg}}{\text{kg}}$
- $T_F \leq T \leq 353 \text{ K}$
- $p = 101325 \text{ Pa}$

Extension to high salinities  
and high temperatures at  
ambient pressure (C)

„normal salinity“  $S_n = 0.03516504 \text{ kg/kg}$

Taken from: IAPWS, Release on the IAPWS Formulation 2008 for the Thermodynamic Properties of Seawater, 2008



# Implementation of the Brine Model by Pitzer

$$G(T, p, m) = m_w G_w(T, p) + n_{\text{Salt}} G_{\text{Salt}}(T, p) + G^{\text{EX}}(T, p, m) + n_{\text{Salt}} \nu RT (\ln m - 1)$$

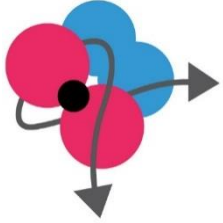
Gibbs Energy from IAPWS-95 (Helmholtz)

Gibbs energy of salt at infinite solution; contains adjustable parameters

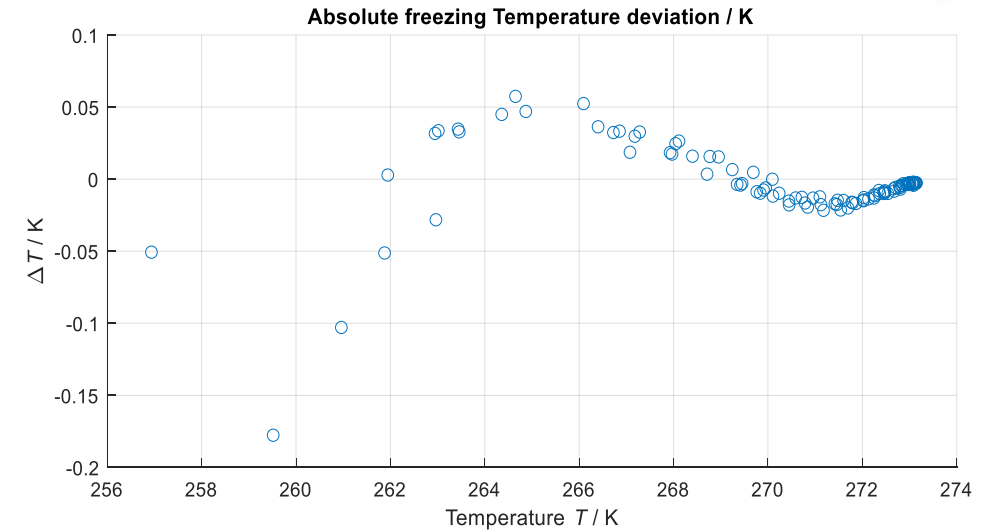
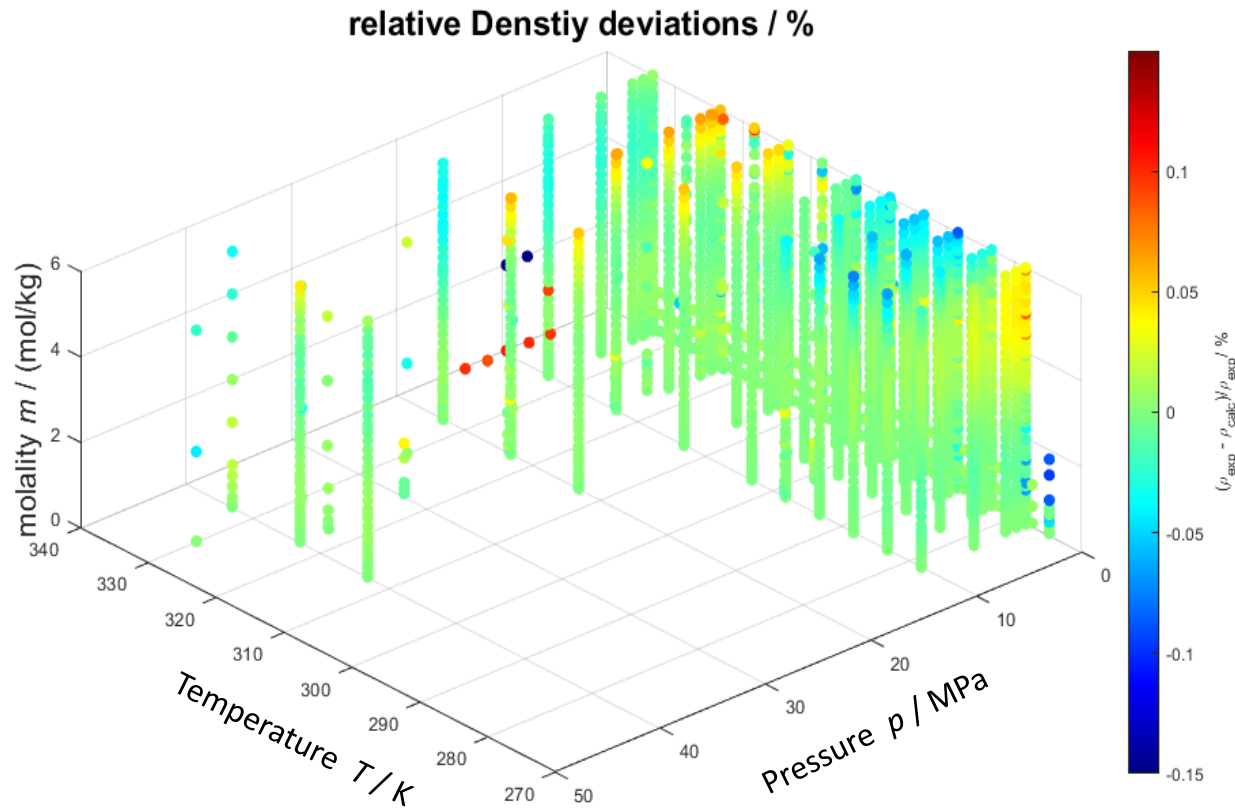
Deybe-Hückel slope; contains dielectric permittivity: Fernández et al., 1997  
Density by IAPWS-95

$$\frac{G^{\text{EX}}}{m_w RT} = -A_\Phi h(I) + 2\nu_M \nu_X [m^2 B_{MX} + m^3 \nu_M z_M C_{MX}]$$

B and C contain adjustable parameters  
Virial expansion for these parameters  
Represent ion-ion interactions

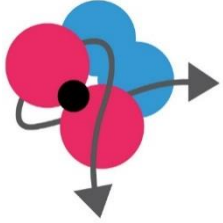


# Results for NaCl Brines



## Pitzer based model ...

- can be extended to other salts
- can be implemented into mixture model based on the routines developed for the seawater model



# Take Away Messages

- Gibbs and Helmholtz energy based EOS have successfully been combined in an accurate multiparameter mixture model
- Pitzer model for the description of brines has been combined with a Helmholtz energy based reference EOS for water (IAPWS-95)
- **Accurate property models used for transport can (soon) be used to describe storage as well**
- **Interface problems (soon to be) overcome**

$$G(T, p, m) = m_w G_w(T, p) + n_{\text{Salt}} G_{\text{Salt}}(T, p) + G^{\text{EX}}(T, p, m) + n_{\text{Salt}} \nu RT (\ln m - 1)$$

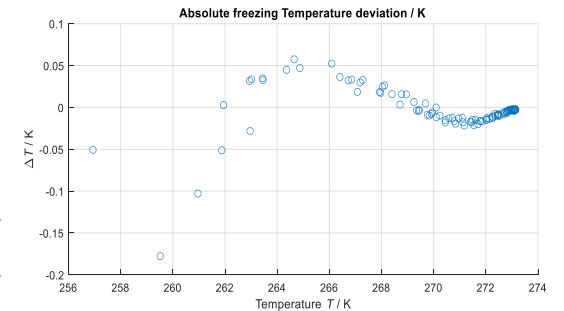
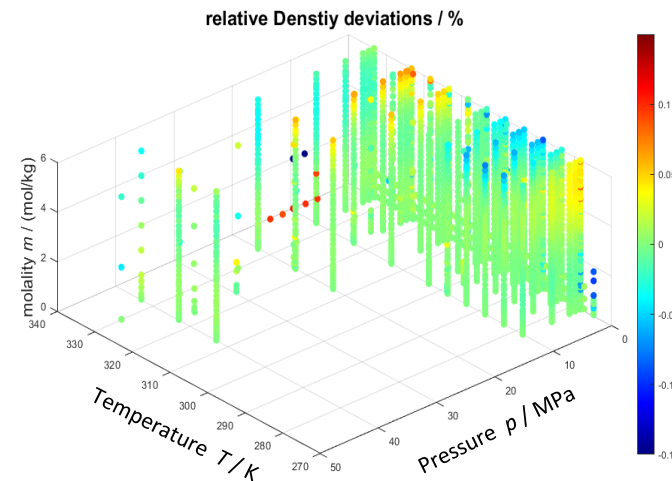
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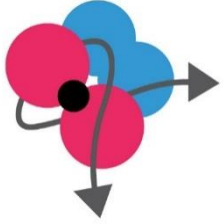
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# Acknowledgement

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