

# FME HighEFF

## Centre for an Energy Efficient and Competitive Industry for the Future



### Deliverable D3.3\_2018.04

#### Thermal storage for improved energy efficiency in the industry

Delivery date: 2018-10-15

Organisation name of lead beneficiary for this deliverable:

**SINTEF Energy Research**

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**Abstract**

Various industries have a vast thermal energy demand in the form of steam, hot water or cooling. The production of steam and hot water is often based on utilization of fossil fuels, while cooling machines with high capacity may be required to cover peaks in cooling demand. At the same time, with increasing share of renewable energy sources in the power grid, industries may have access to green power with highly fluctuating prices. Moreover, there is a large potential for utilization of surplus heat from the industry.

This study presents three potential applications of thermal energy storage (TES) to improve energy efficiency and reduce emissions in the industry: (i) large-scale steam storage to be used in the Bayer process for production of alumina; (ii) cold TES for food industry; and (iii) hot water accumulator tank in a district heating (DH) system based on the use of industrial waste heat. Each application is being studied and developed under FME HighEFF, research centre for an energy efficient and competitive industry for the future.

The production of alumina from bauxite is based on the Bayer process, with a high demand for steam, traditionally produced by using fossil fuels. The use of fossil fuels could be replaced by electricity from fluctuating renewable sources, concentrated solar power (CSP), or high-temperature heat pumps utilizing industrial waste heat. In either case, large-scale steam storage able to deliver steam at high volume flow rates is required, currently not available commercially. For the present case, the process requirements are steam at 15 bar and a flow rate up to 1200 t/h. The desired storage capacity is up to 7800 MWh. Different storage alternatives, capable of meeting this requirement, will be discussed.

A large chicken slaughter house is under construction in Orkanger, Norway. The plant will have huge energy demand in the form of cooling and hot water, and access to renewable power from a nearby wind power plant. To be able to utilize green electricity from the fluctuating power market, a novel cold TES system with a storage capacity of 11 MWh utilizing CO<sub>2</sub> as the heat transfer fluid will be installed, in addition to accumulator tanks for hot water. The TES system is estimated to reduce the peak power demand by 20 %.

Finally, the DH production in Mo i Rana, Norway, is based on waste heat recovery from off-gases of a nearby ferrosilicon production plant. Even if the amount of waste heat available exceeds the heat demand in Mo i Rana by far, costly peak heating sources are required to cover peak heating demands due to large fluctuations in both availability and demand of heat. By the use of thermal storage and optimal control, the use of costly peak heating sources may be reduced or even avoided. Initial simulation results from a dynamic model of the waste heat recovery system incorporating thermal storage with a capacity of 9 MWh and optimal control will be presented.



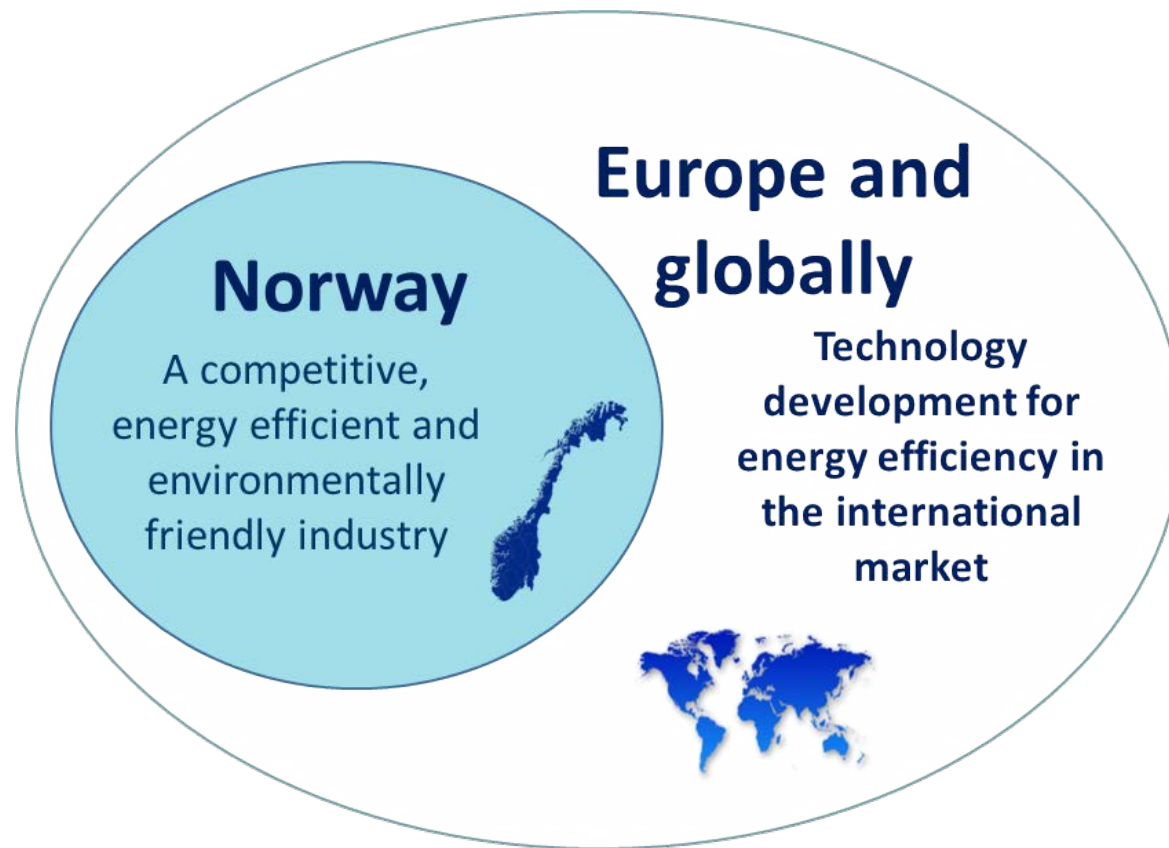
# Thermal storage for improved energy efficiency in the industry

Hanne Kauko, Håkon Selvnes, Brage R. Knudsen, Armin Hafner and Petter Nekså

10th KIFEE Symposium 5.-8.10.2018

# HighEFF Vision

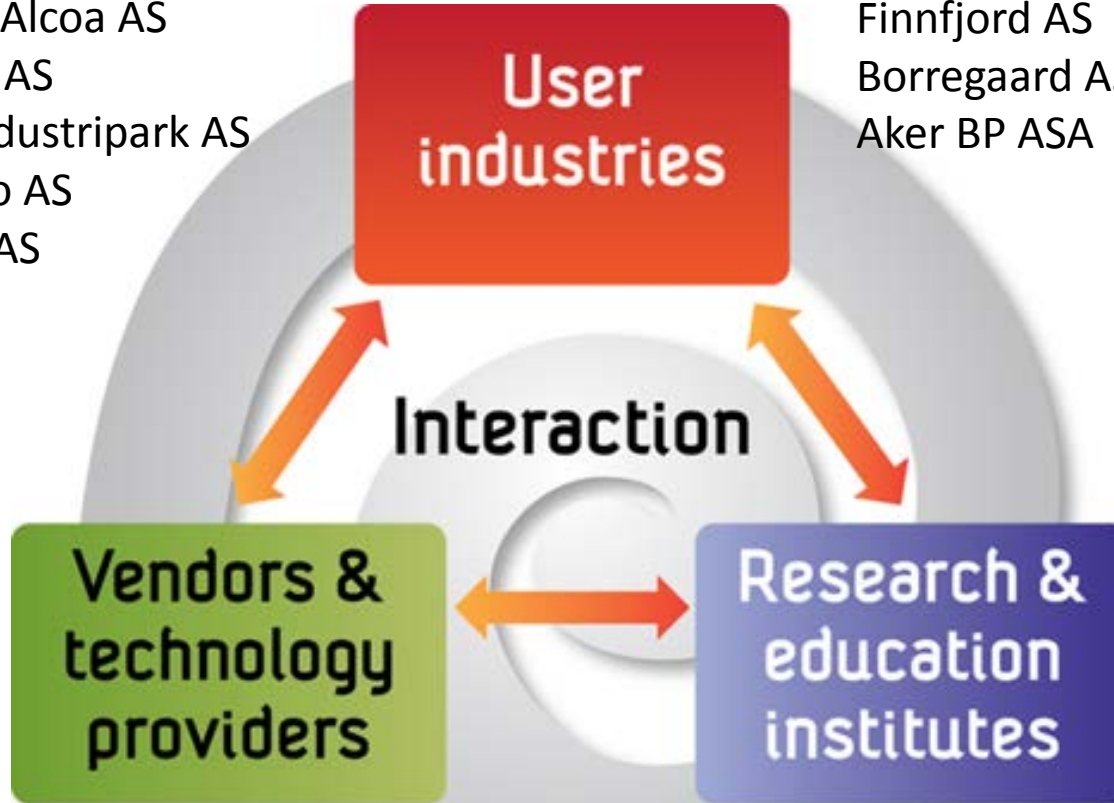
Joint effort for creating a competitive, energy efficient and environmental friendly industry for the future



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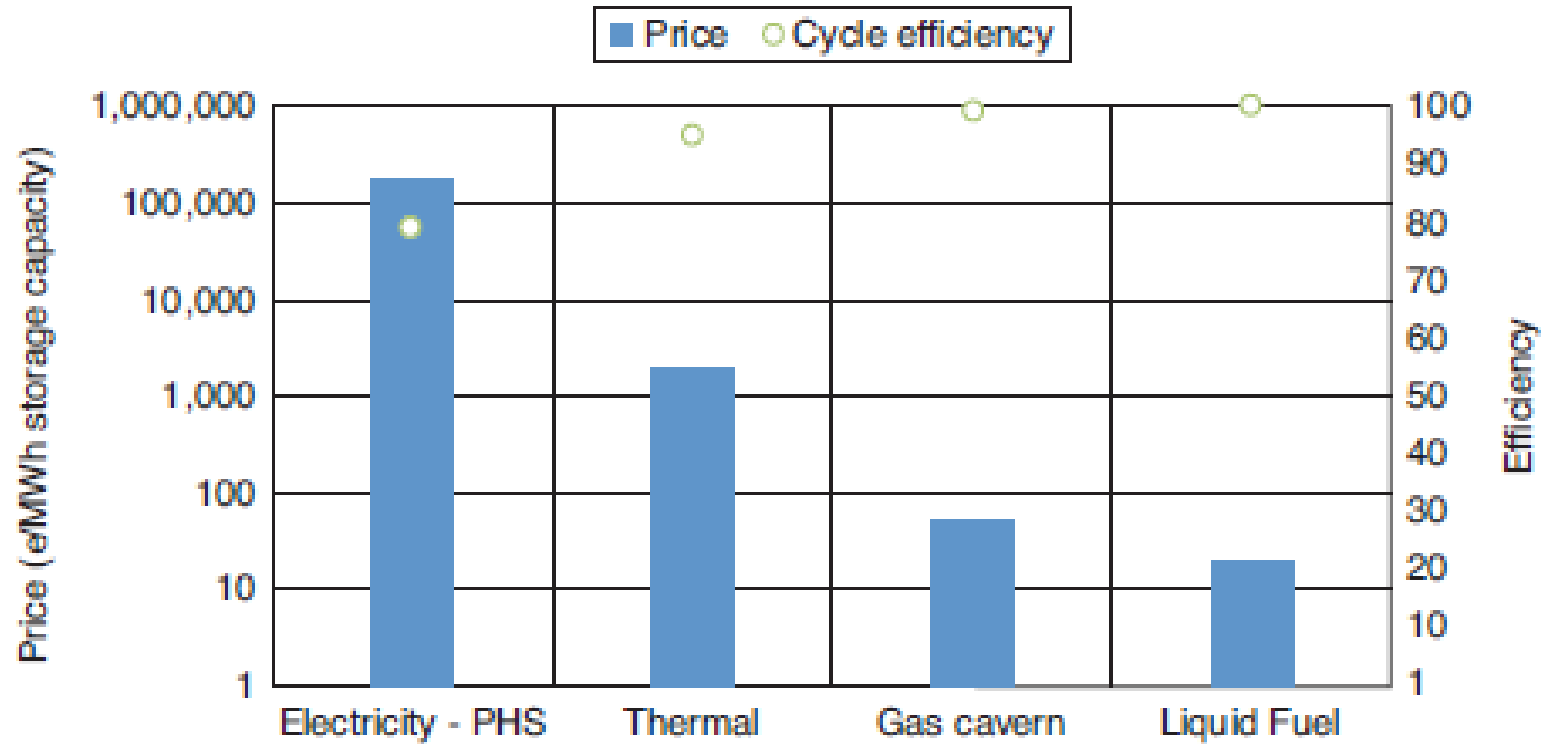
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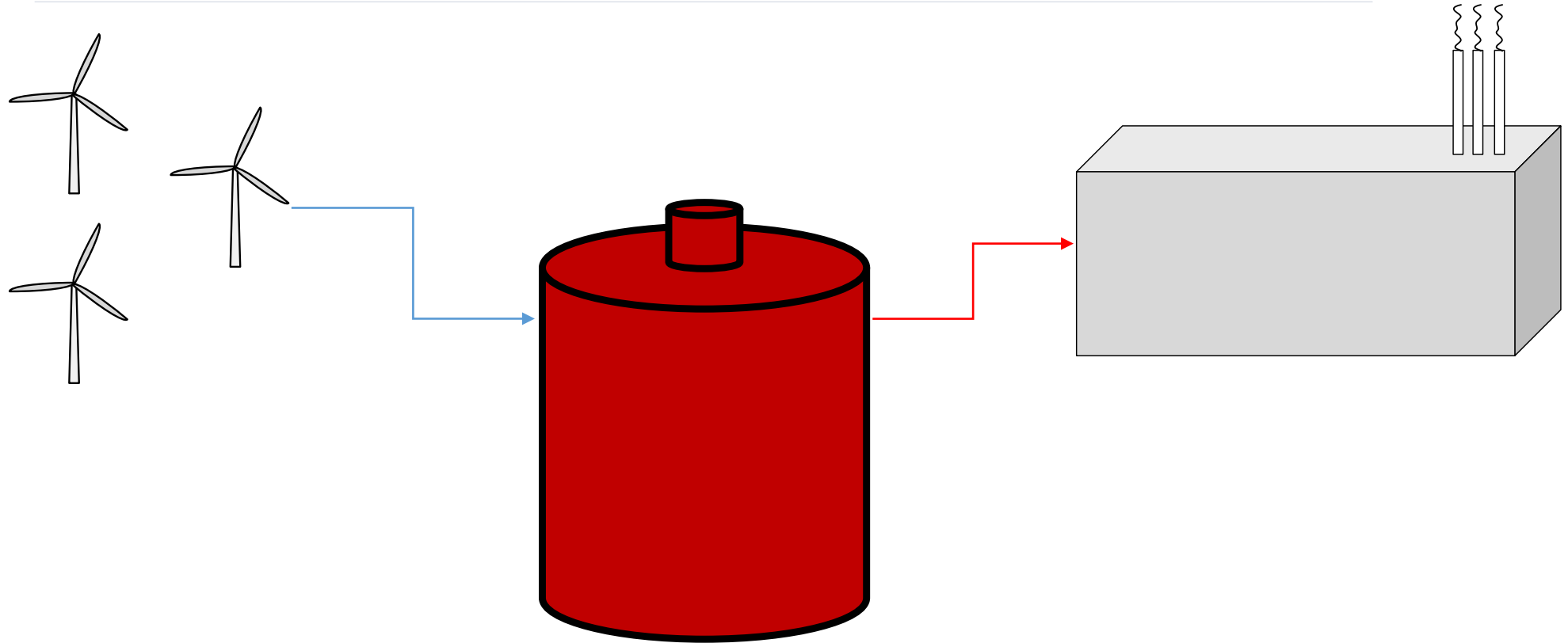




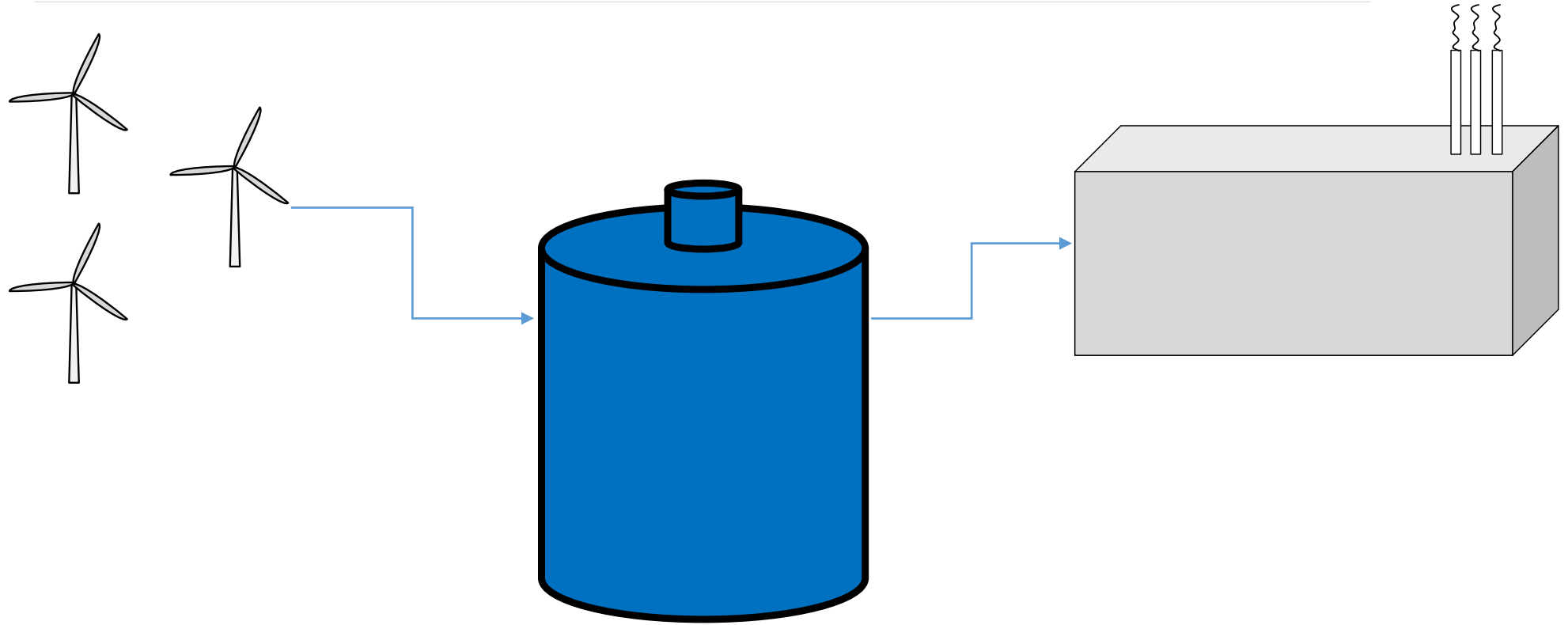


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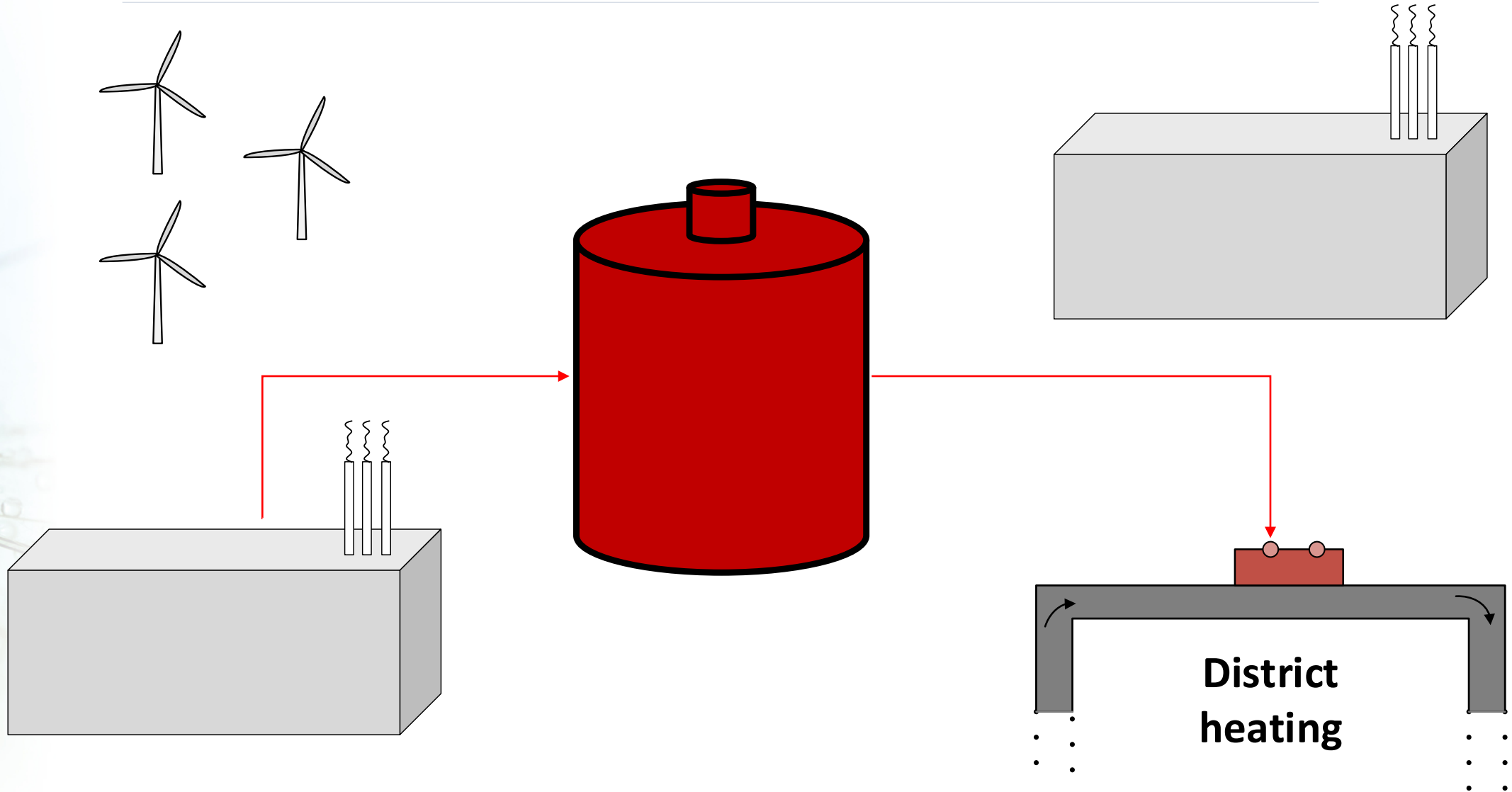
# 3 cases for application of TES in the industry



# 3 cases for application of TES in the industry



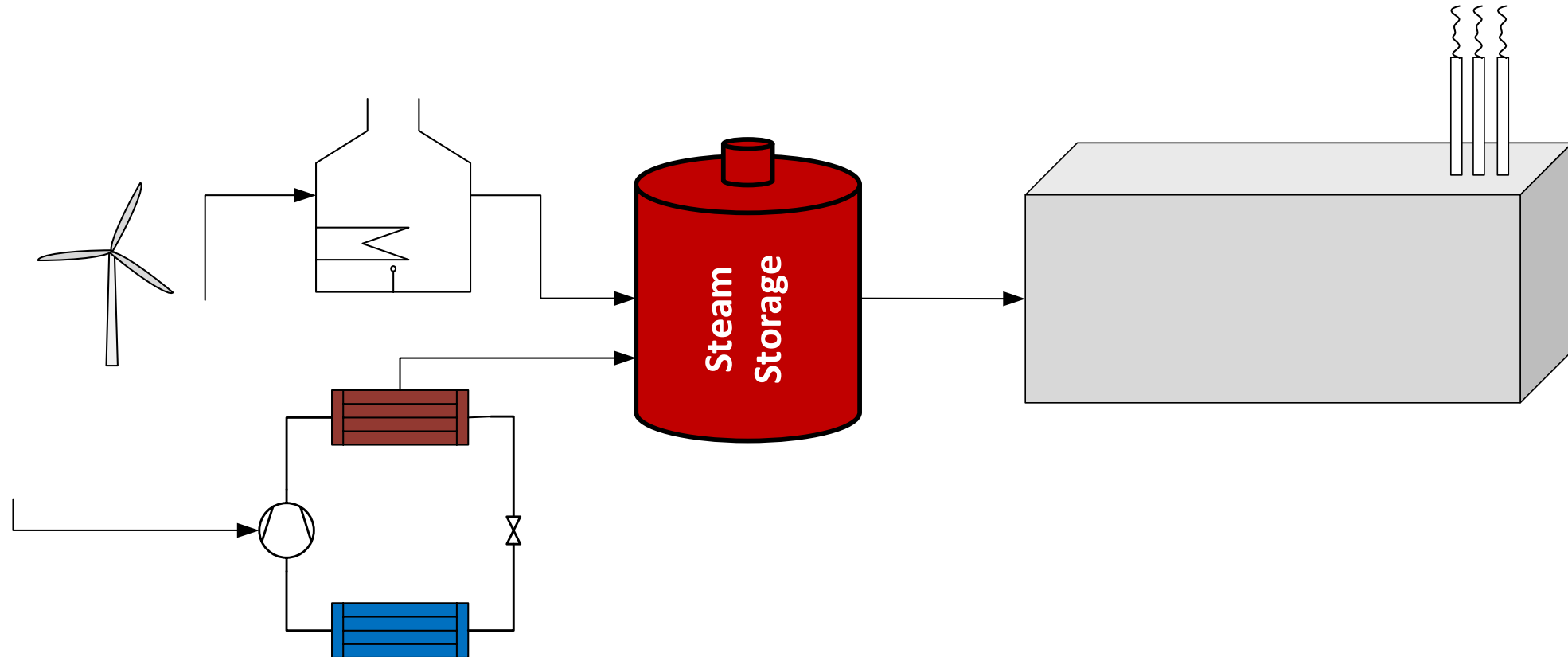
# 3 cases for application of TES in the industry



# Case 1: Steam storage for the metal industry

Production of alumina from Bauxite through the Bayer process

- Steam demand up to 1000 t/h at 150 °C, 15 bar
- Green energy available from a fluctuating power market
- Large scale storage needed



# Ruths Steam Storage

## Characteristics

Storage medium: Water, steel

Direct storage

Variable power to energy ratio

Storage density:

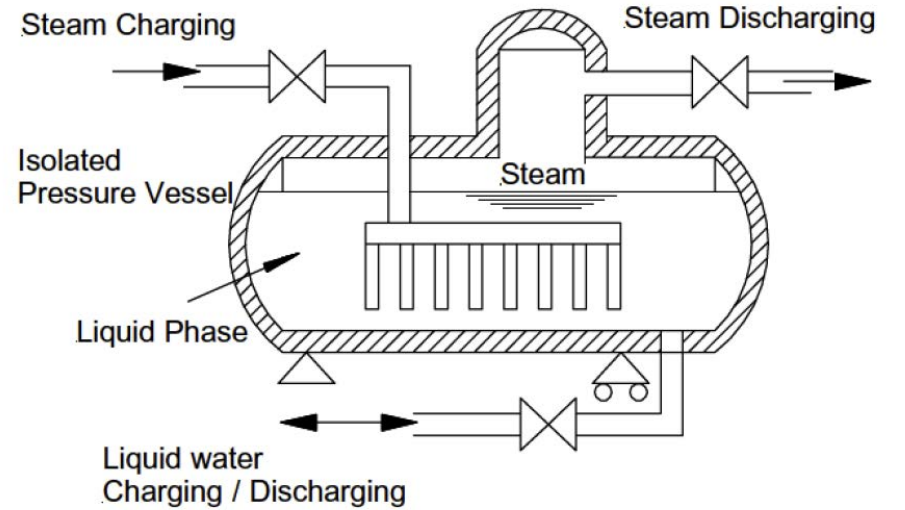
~ 40 kWh/m<sup>3</sup> at 30 bars

~ 31 kWh/m<sup>3</sup> at 100 bars

Costs: 4 €/tons of water, 6000 €/t steel

## Pros

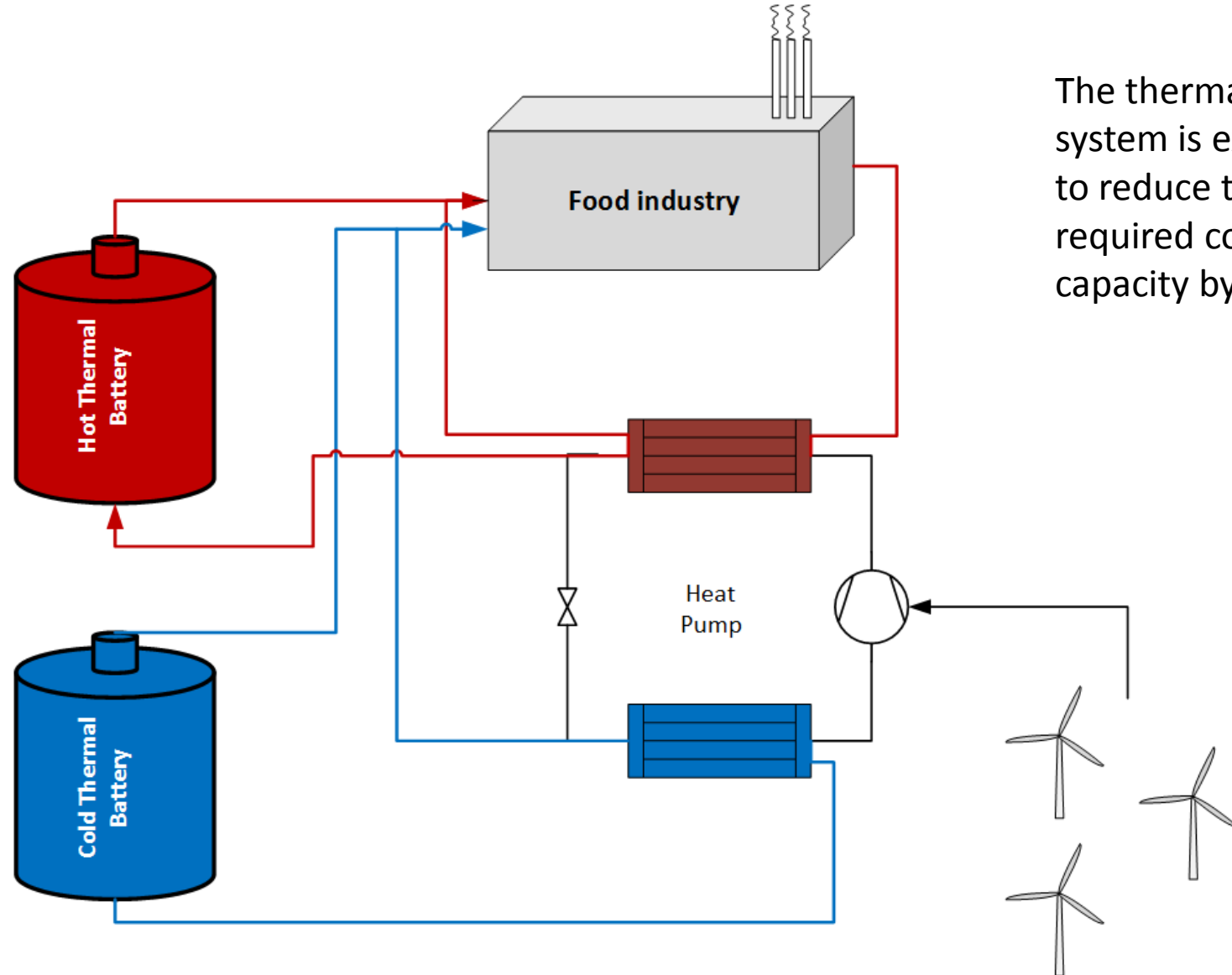
- Simple
- Commercially available
- Good for short time storage with high powers



## Cons

- Low storage density at high pressures
- High costs of steel
- Not large scale storage and longer time scales

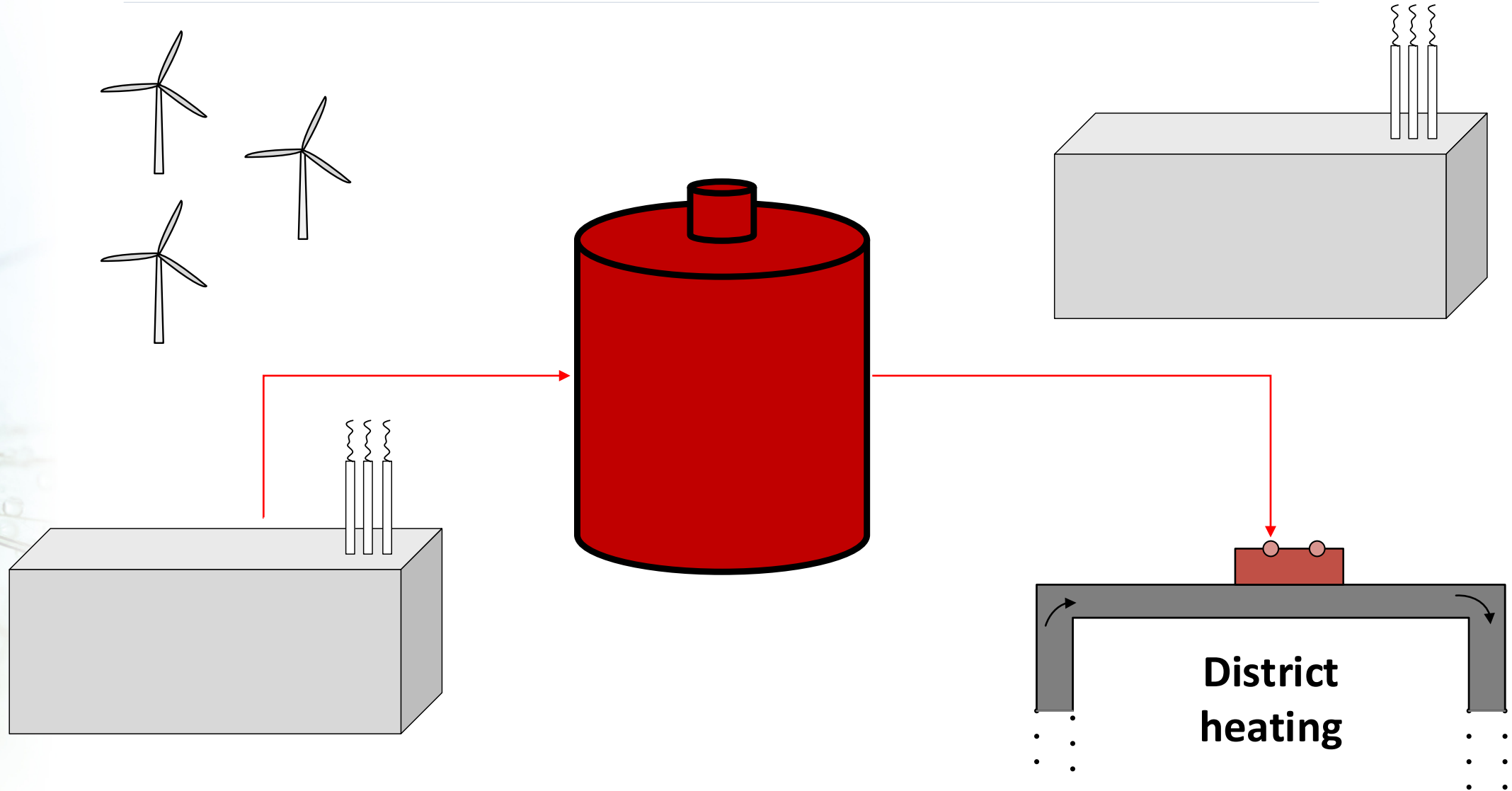
## Case 2: Cold TES for the Food Industry



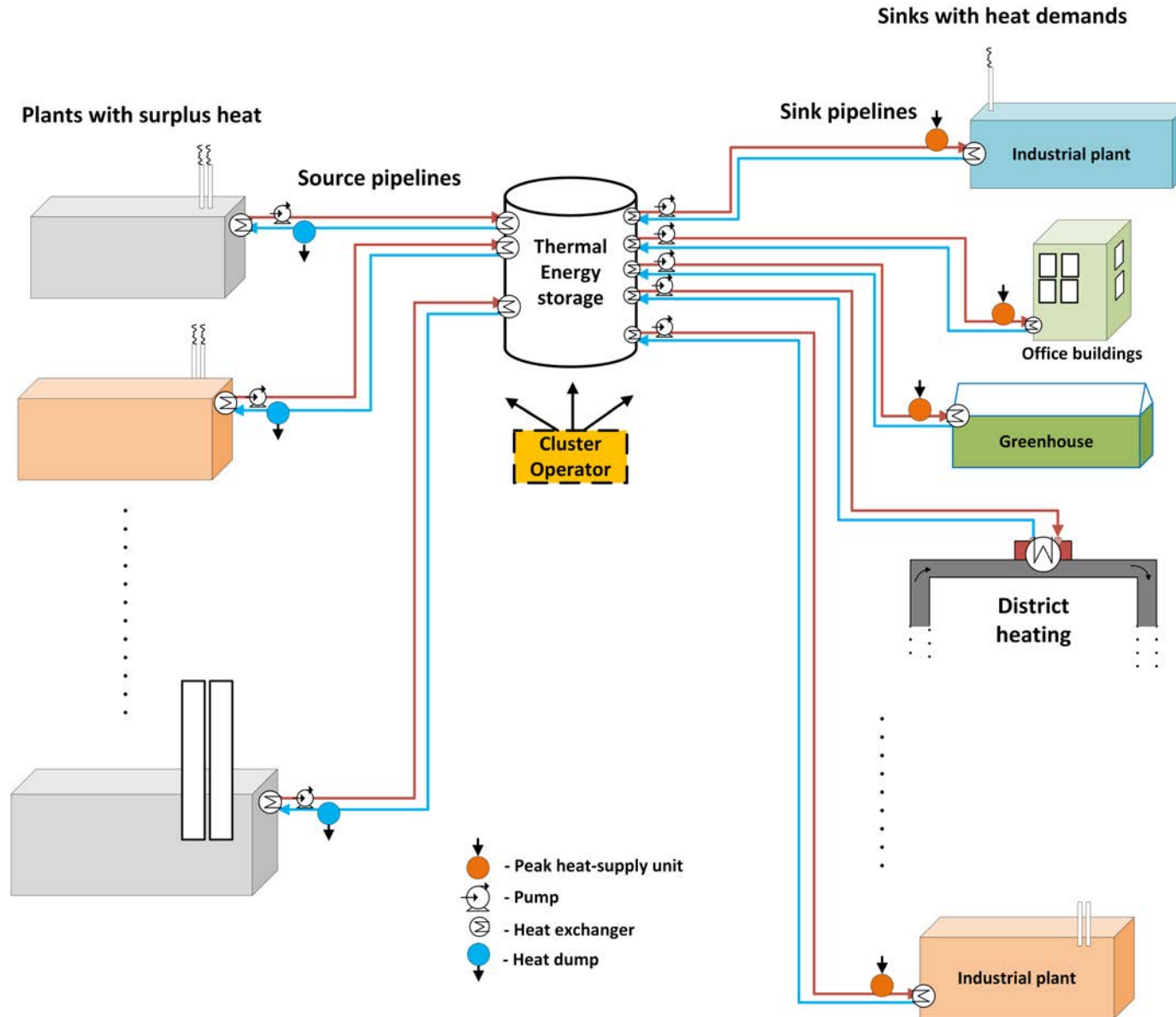
The thermal storage system is expected to reduce the required compressor capacity by **20 %**.



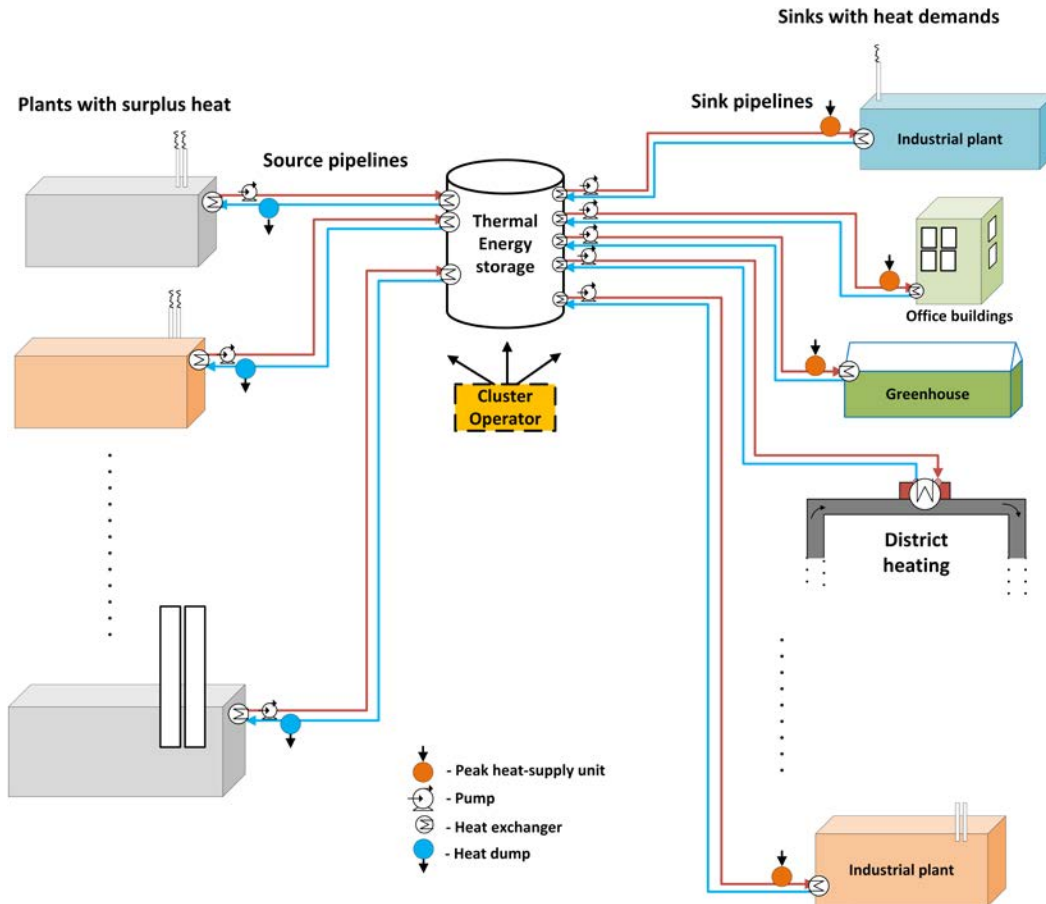
# 3 cases for application of TES in the industry



# Case 3: TES + optimal control for industrial clusters



# TES + optimal control for industrial clusters



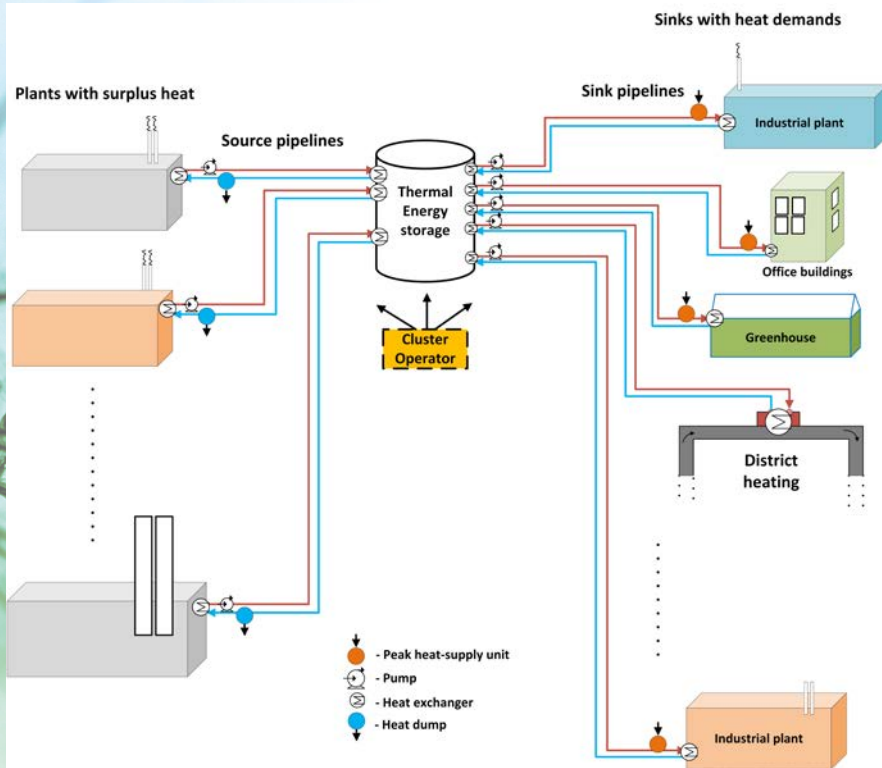
## Challenges

- Mismatch in availability vs. demand
- Surplus heat sources with different temperature levels
- Costly peak heating sources

## Goals

- Maximize utilization of surplus heat with thermal energy storage (TES)
- Minimize use of peak heating sources
- Minimize heat dumping
- Predict fluctuations in demand and availability of heat

# The optimization problem



Peak heating supply

Dumped surplus heat

Pump flow velocity

$$\min_{v_j^{\text{pump}}, Q_j^{\text{peak}}, Q_i^{\text{hd}}} \int_{t_0}^{t_f} \left( \sum_{j \in \mathcal{J}} Q_j^{\text{peak}}(t) + \gamma_1 \sum_{i \in \mathcal{I}} Q_i^{\text{hd}}(t)^2 + \gamma_2 \sum_{j \in \mathcal{J}} v_j^{\text{pump}}(t)^2 \right) dt$$

Objective function

$$\text{s.t. } |Q_j^{\text{del}}(t) - \bar{Q}_j^{\text{demand}}(t)| \leq \delta_j \bar{Q}_j^{\text{demand}}(t),$$

Satisfaction of demand

$$Q_j^{\text{del}}(t) := Q_j^{\text{TES, out}}(t) - Q_j^{\text{loss}}(t) + Q_j^{\text{peak}}(t),$$

$$0 \leq v_j^{\text{pump}}(t) \leq \bar{v}_j^{\text{pump}}$$

$$Q_j^{\text{peak}}(t) \geq 0,$$

$$Q_i^{\text{hd}}(t) \leq 0,$$

Bounds on control inputs

$$T^{\text{TES}}(t) \leq \bar{T}^{\text{TES, max}}$$

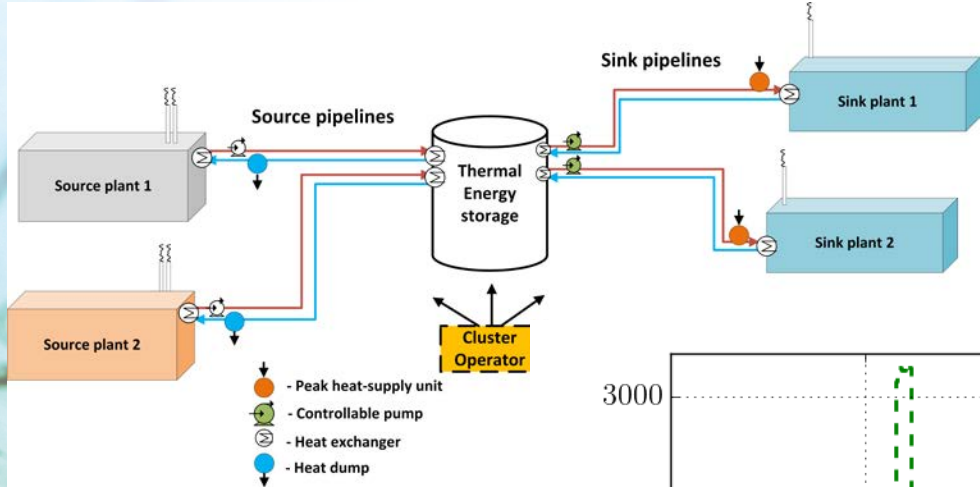
$$T_{j,p}^{\text{pipe-source}}(t) \leq \bar{T}_{c,i}^{\text{source}},$$

System constraints

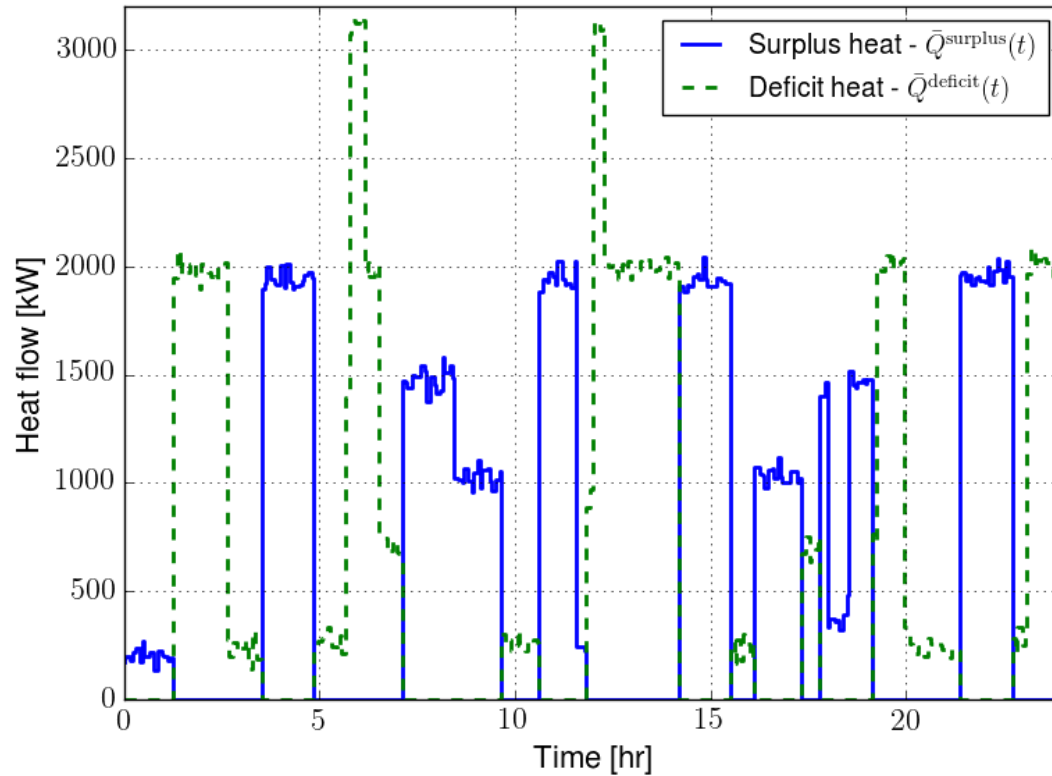
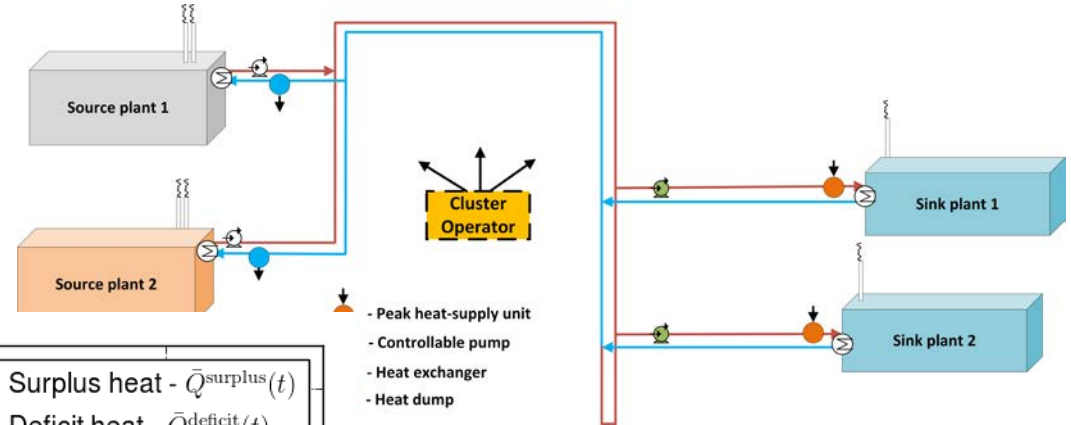
Dynamic models of pipelines, HEXs and TES units

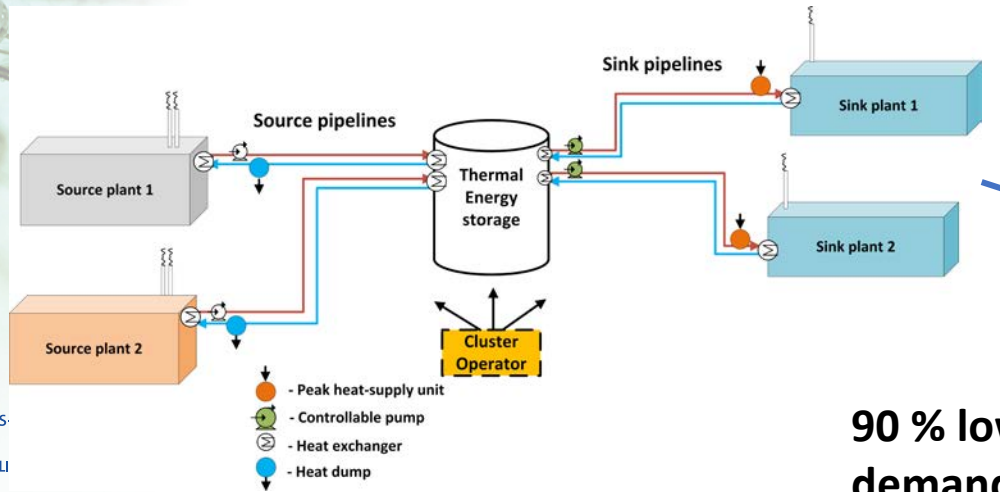
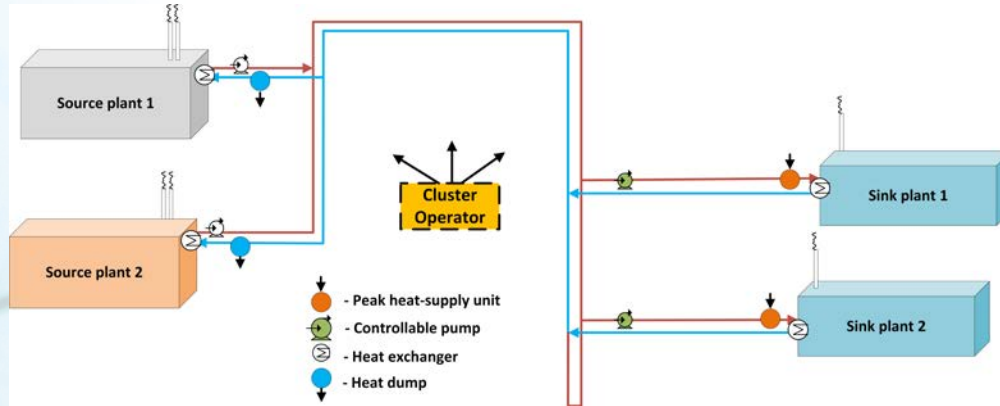
System unit models

# Case study

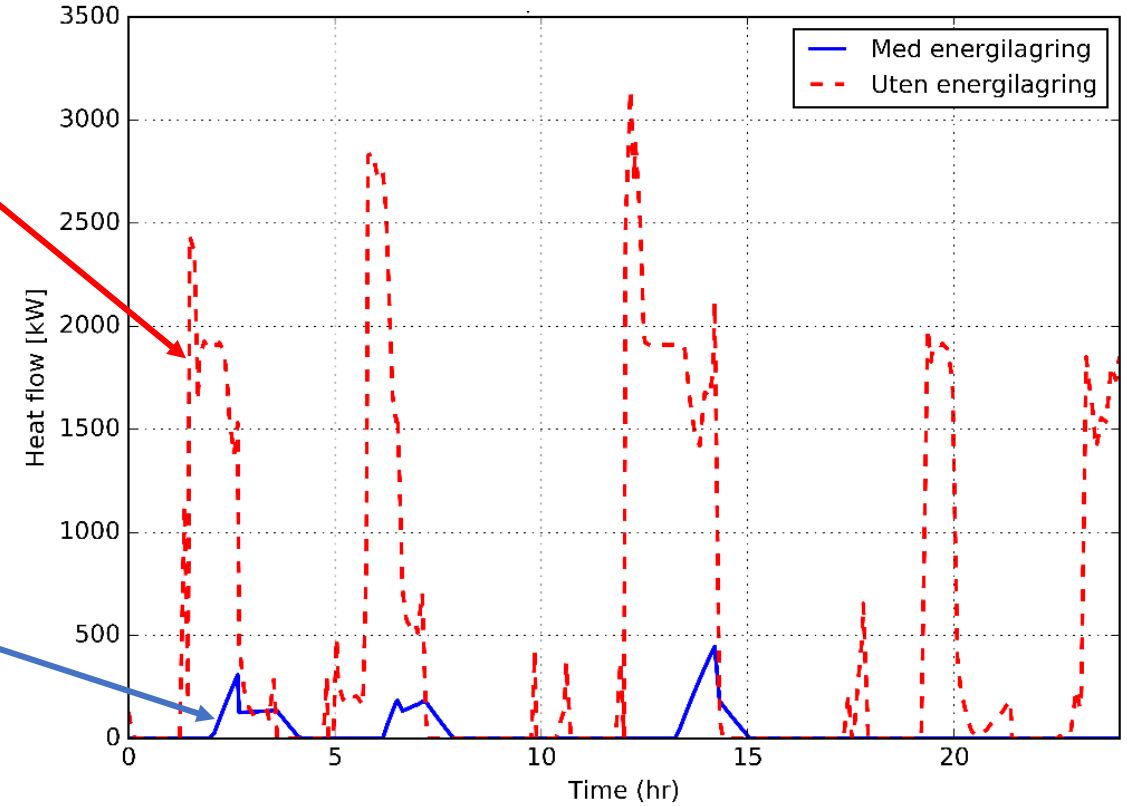


V.S.



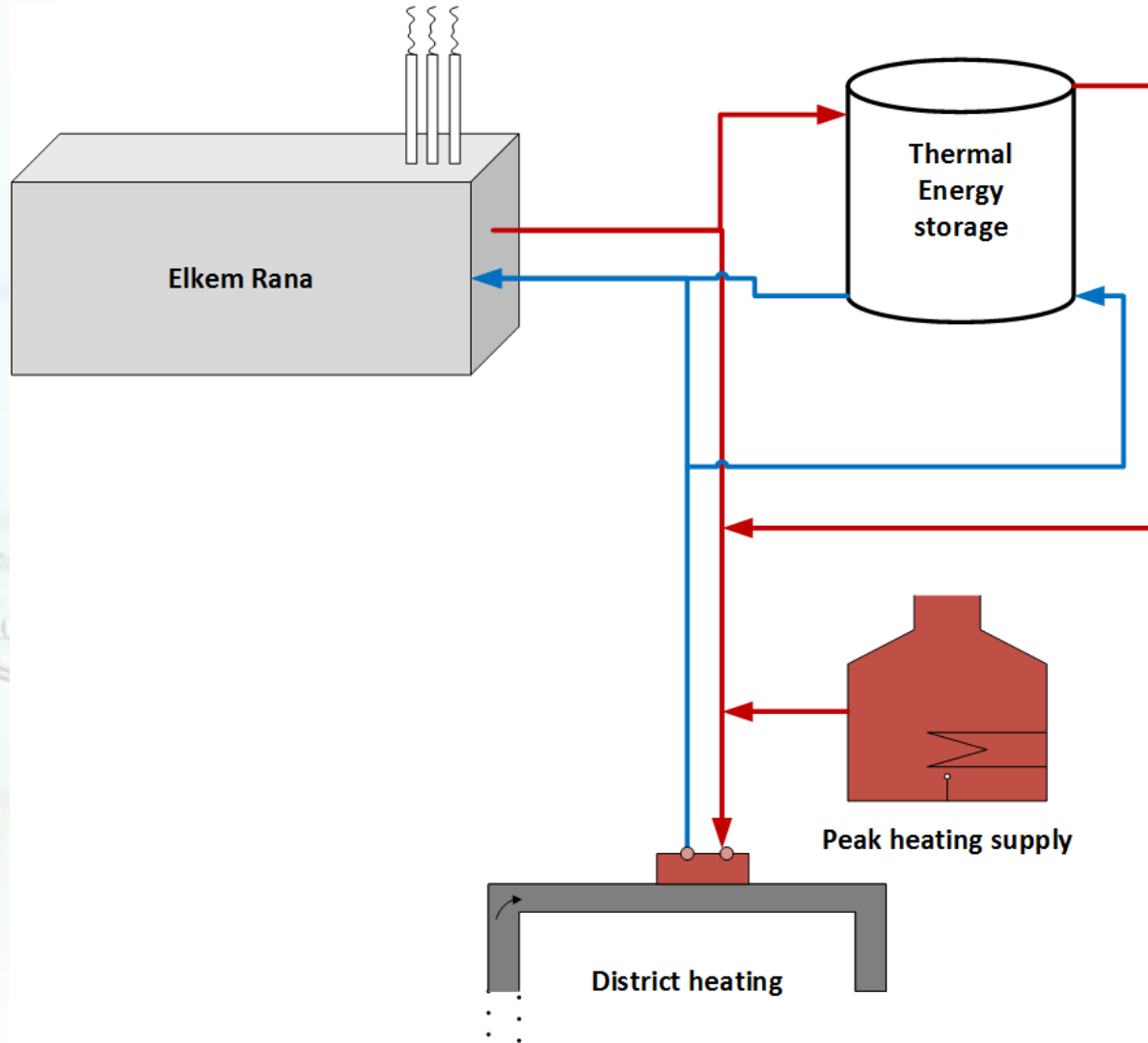


Delivered peak heating over 24 hours



**90 % lower peak heating demand when TES is applied.**

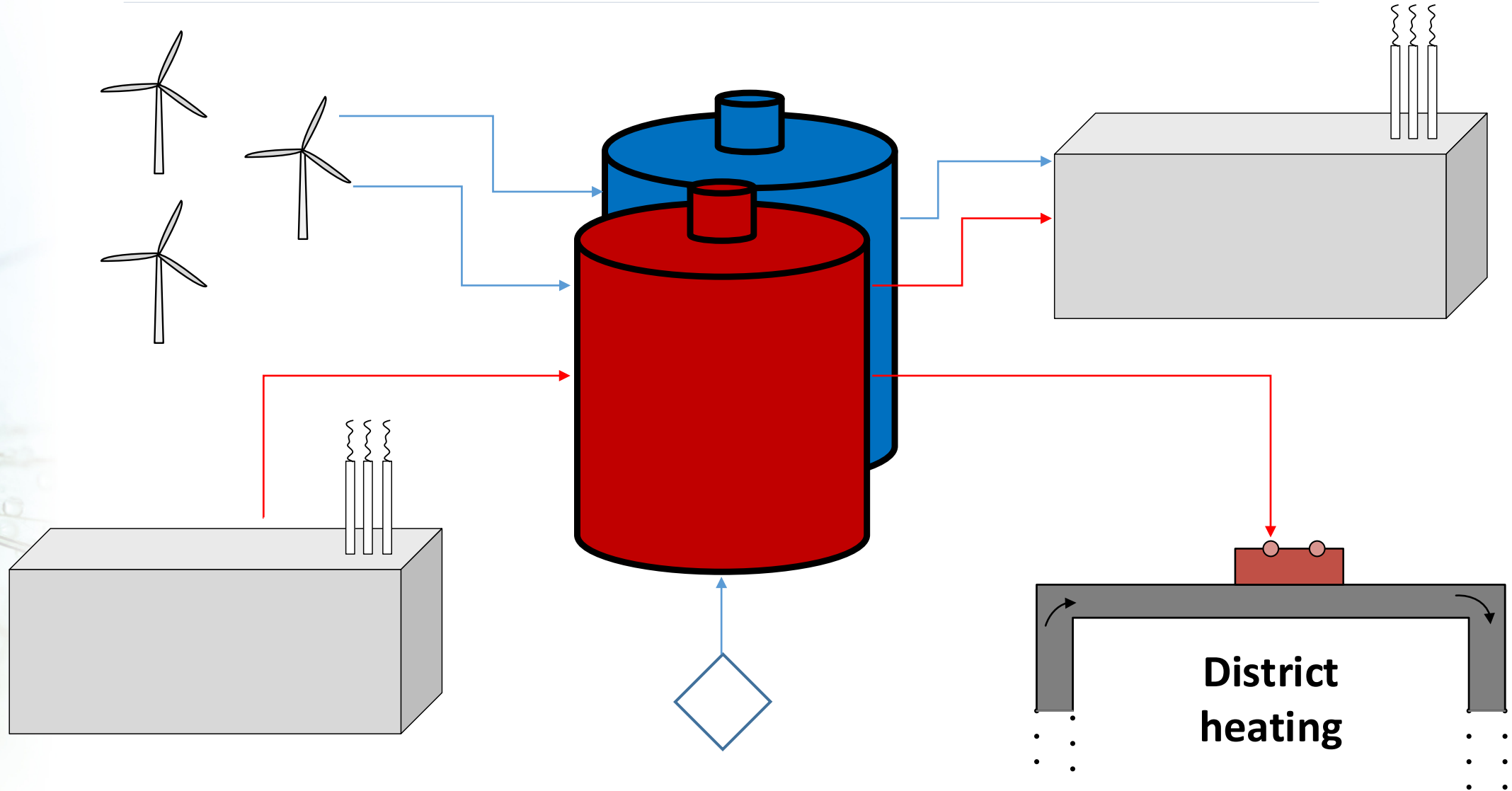
# Potential for TES at Mo Industrial Park



## Background:

- 85 GWh district heating (DH) annually
- 90 % of the DH from surplus heat from a FeSi plant
  - Remaining covered by peak heating boilers utilizing CO (9%) or electricity (1 %)
- Predictable peaks in the demand during the morning and afternoon

# Summary and Conclusions







Thank you for your attention.

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