

# FME HighEFF

## Centre for an Energy Efficient and Competitive Industry for the Future



### Deliverable D3.1\_2017\_04

#### Numerical framework for power cycle simulation and optimization

Delivery date: 2017-11-30

Organisation name of lead beneficiary for this deliverable:

**SINTEF Energy Research**

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#### Dissemination Level

|    |   |   |
|----|---|---|
| PU | Public  | X |
| RE | Restricted to a group specified by the consortium |   |

|                            |  |
|----------------------------|--|
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\*<sup>1</sup>) *The quality assurance and approval of HighEFF deliverables and publications have to follow the established procedure. The procedure can be found in the HighEFF eRoom in the folder "Administrative > Procedures".*

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|                |                        |  |
|                |                        |  |

| <b>Abstract</b> |
|-----------------|
|                 |

# Numerical framework for power cycle simulation and optimization - FlexCS

```

define BCUMP 11

int bcycle () {

  FCSSystem *system = FCSSystem_create();
  initSolver(system);

  system->nrefstreams = bcycleInitInletStreams(system);
  initComponents(system);
  FCSSystem_simpleReport(system);
  initVariables(system);
  FCSSystem_initLogFiles(system);

  solveSystem(system);

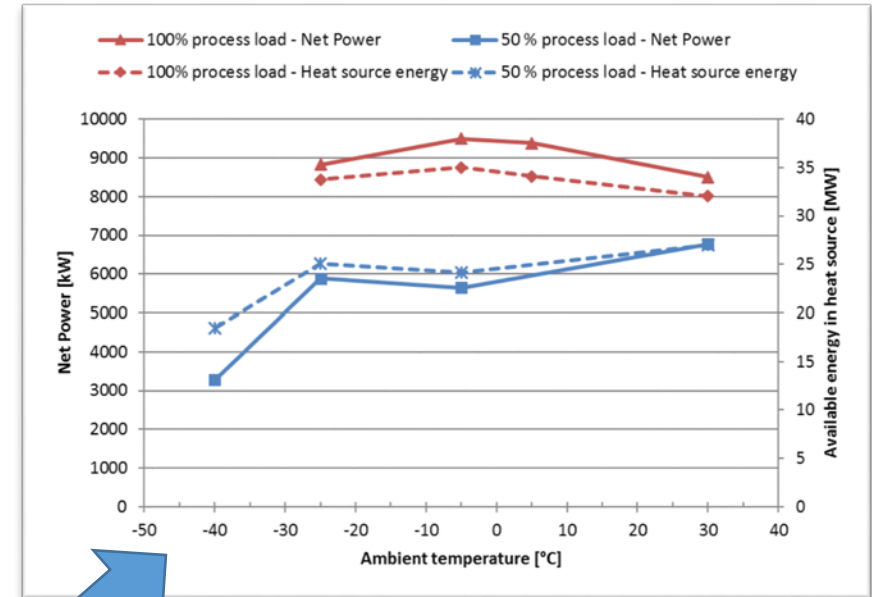
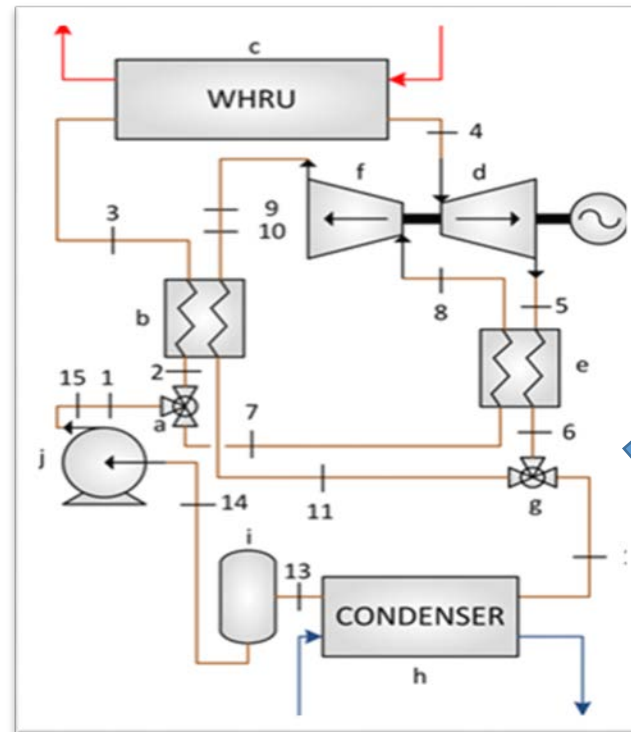
  if (!offDesignExp.on) {
    FCSExpander_SaveExpanderDesign(system->expanderA->buf[0]);
    FCSExpander_SaveExpanderDesign(system->expanderA->buf[1]);
  }

  FILE *systemSimpleReport;
  FILE *systemReport;
  systemSimpleReport = fopen("systemstreamresults.res", "w");
  systemReport = fopen("systemreport.res", "w");
  FCSSystem_writeSimpleReport(system, systemSimpleReport);
  FCSSystem_writeFullReport(system, systemReport);
  fclose(systemSimpleReport);
  fclose(systemReport);

  if (tabulatesource.on) {
    int istream;
    istream = FCSSystem_getInletIndex(system, "sourceinlet");
    if (istream < 0) AAAUtil_panic("destroy: sourceInlet not found");
    FCSSystem *sourceInlet = system->streamA->buf[istream];
    FHNTermotab_destroy(sourceInlet->node->thermotab);
    sourceInlet->node->thermotab == AAA_NULL;
  }
  FCSSystem_destroy(system);

  AAAMemory_info();
}

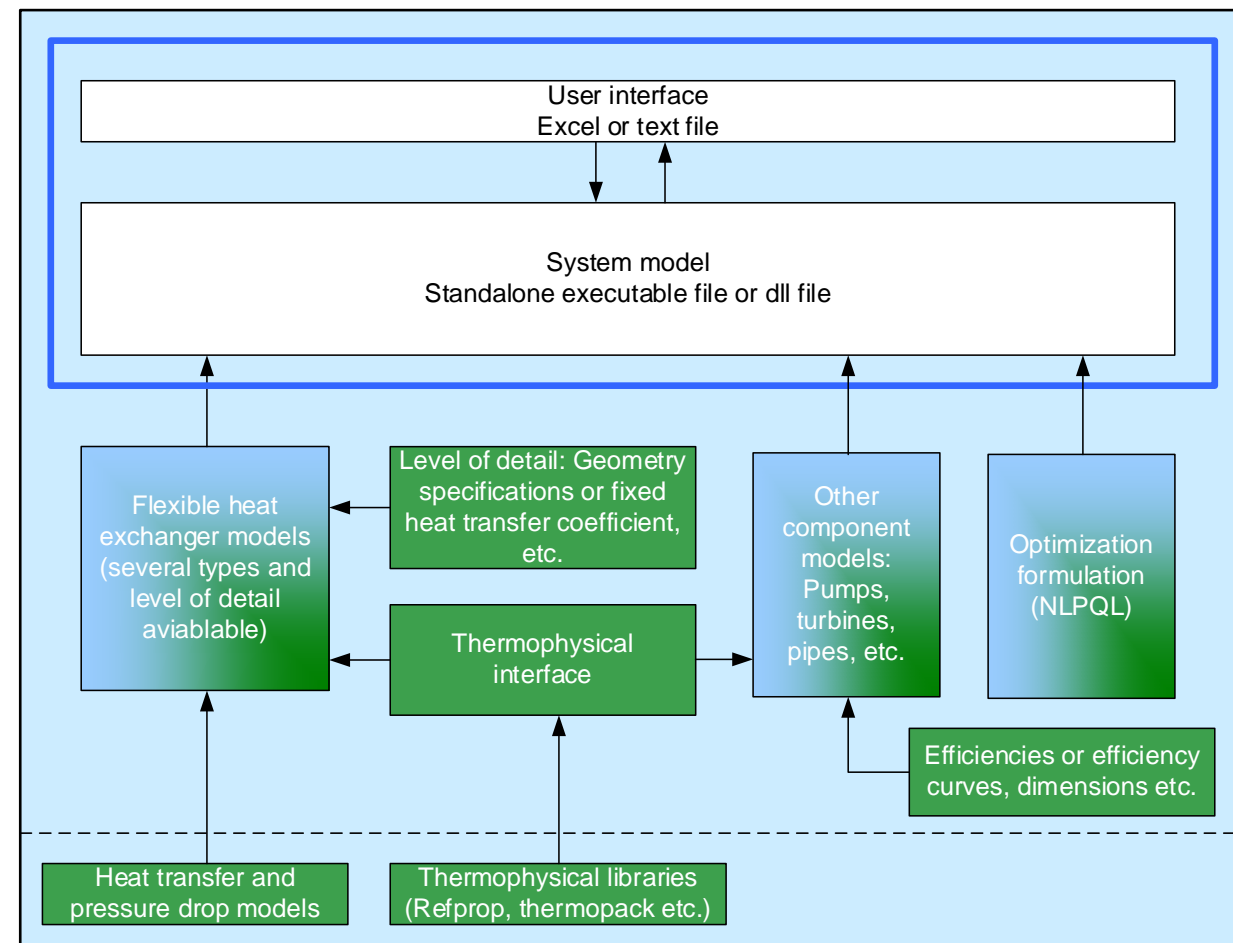
```



# The numerical framework: Flexible cycle simulator (FlexCS)

What is FlexCS?

- In-house "Cycle simulator" with flexible building blocks/component models
- Access to fluid properties, correlations for heat transfer and pressure drop and numerical methods
- Medium-high user threshold to assemble models (code written in C)
- Low-Medium user threshold to run parametrized models (user interface is text file or Excel)
- Cycle model can choose HX-models of different levels of detail according to the task

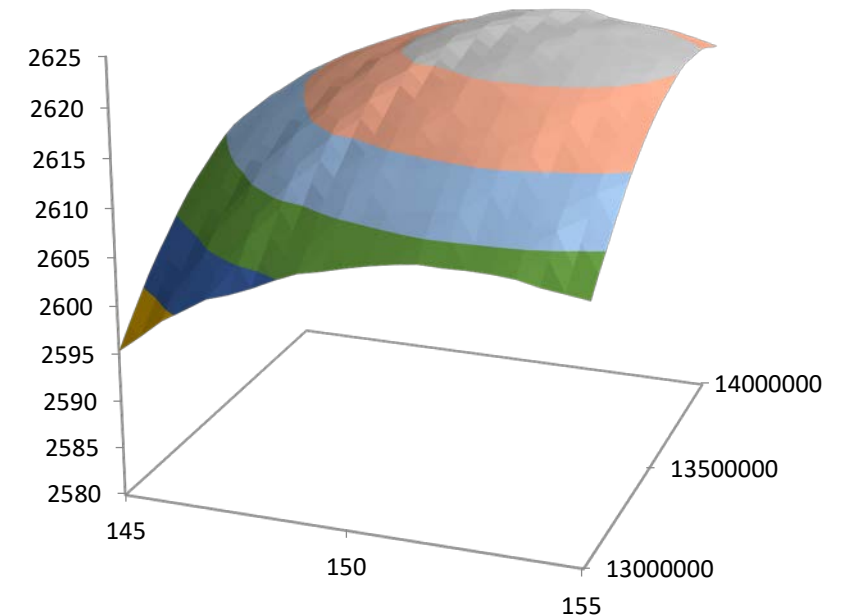
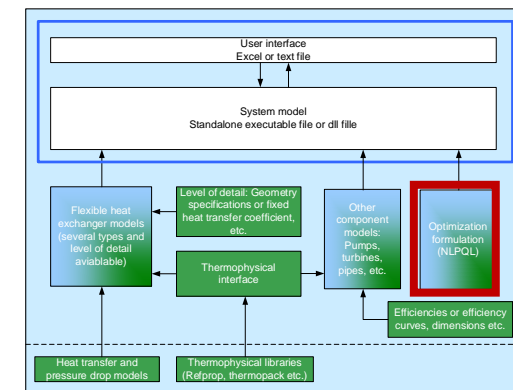


# Why rely on in-house models?

- Required features not available in commercial software
  - Components models
  - System models
  - Off-design behaviour
  - Optimization
- Tailored to best address the problem
  - Direct implementation of state-of-the-art knowledge (correlations, fluid properties)
  - Models for novel and new components, adding new correlations when required
  - Free choice of optimization object function and constraints
- Full control of problem formulation and solution
  - Equations describing fundamental behaviour
  - Correlations for heat transfer, pressure drop, void fraction
  - Parameterization and discretization
- Our in-house models are built to predict behaviour of fluids, components and systems
- In-house models are used when available commercial software is inadequate

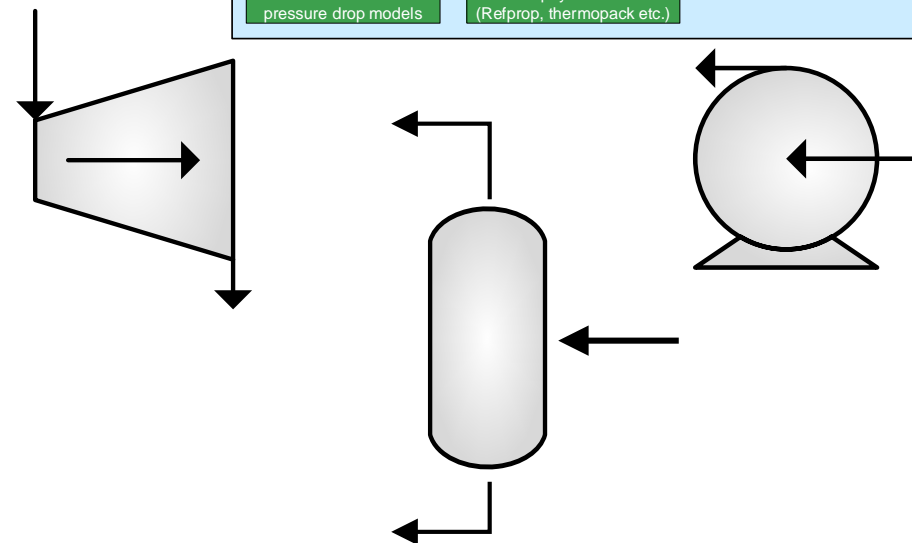
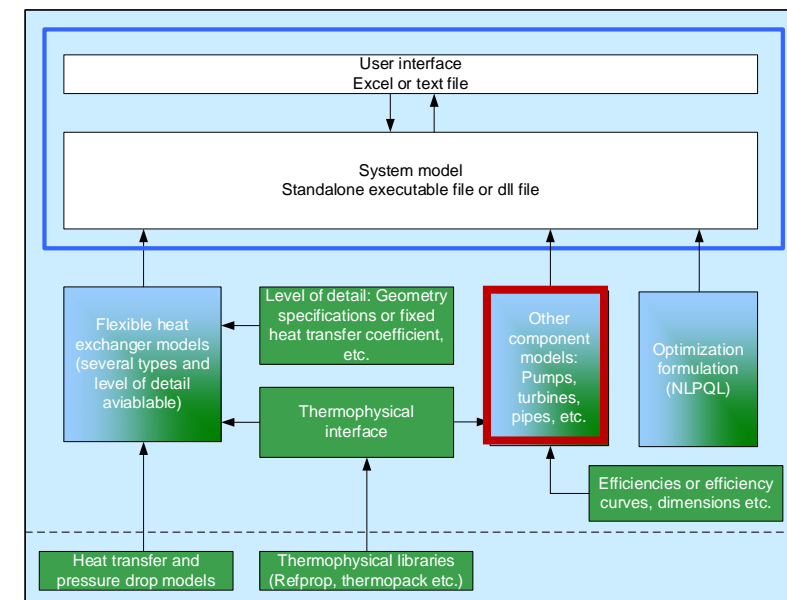
## System Solver – NLPQL\*

- A constrained non-linear optimisation solver
- Applied in all power cycle models in FlexCS
  - For balancing the system and optimizing the process/HX geometry
- Typical variables: Working fluid mass flow, pressure levels, heat exchanger geometry
- Typical constraints:
  - Avoid two-phase expansion, ensure a closed cycle, maximum allowed heat exchanger area
- Flexible selection of objective function
  - Minimize weight, maximize net power etc.



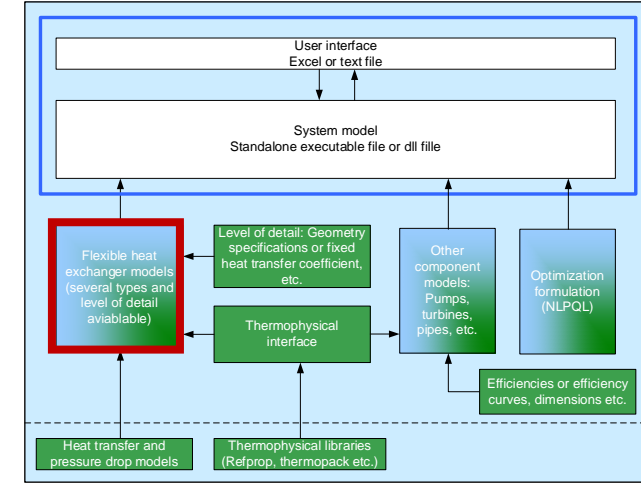
# Component models (in addition to heat exchangers)

- Compressors / Pump
  - Isentropic and isochoric
- Expanders / Turbine (Three alternatives)
  - Fixed isentropic efficiency
  - Efficiency curve for a radial expander with Variable Inlet Guide Vanes (VIGV)
  - 1D radial turbine model under development
- Valve
  - Isenthalpic
- Separators
  - Liquid receiver, Suction drum, Flash tank
- Piping
  - FlexHX tube model
- Mixers and splitters
  - Adiabatic

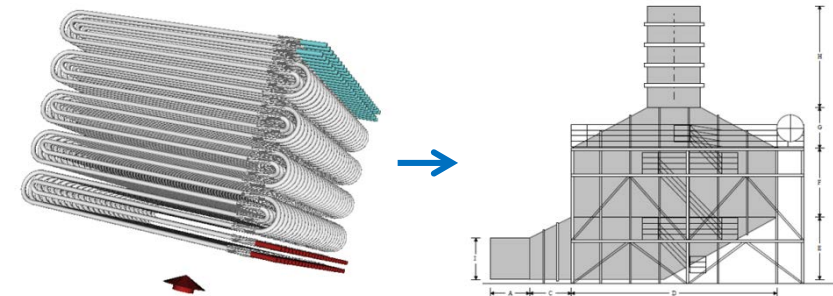


# Flexible heat exchanger model selection

- Simple heat exchanger models
  - Pinch point or UA-based models
- Simplified geometry based models
  - Independent of heat exchanger type
  - Characterize the heat exchanger by:
    - Tube diameter, length and number of tubes
  - Obtain estimates for local heat transfer coefficients and pressure drop and total heat transfer area
- FlexHX – flexible heat exchanger library\*
  - Detailed models based on geometry and local fluid behaviour.
  - Heat exchanger types:
    - Printed circuit, Plate type, Shell and tube, Tube-in-fin, Finned tube, ...



A detailed model of a finned tube waste heat recovery unit



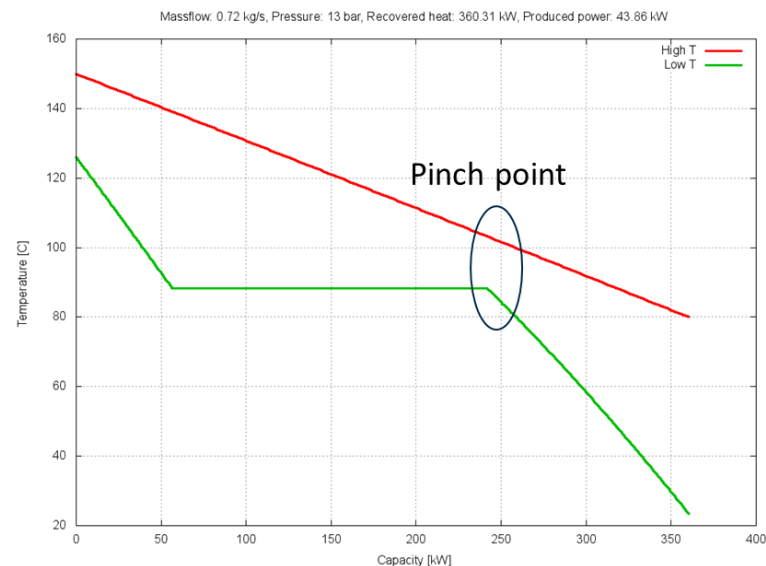
Skaugen Geir, et. al (2014). DESIGN AND OPTIMIZATION OF WASTE HEAT RECOVERY UNIT USING CARBON DIOXIDE AS COOLING FLUID. ASME Power 2014 Conference

\* Skaugen G., Kolsaker K., Walnum H. T., Wilhelmsen Ø. (2013) A flexible and robust modelling framework for multi-stream heat exchangers. *Computers and Chemical Engineering* 49, 95–104.

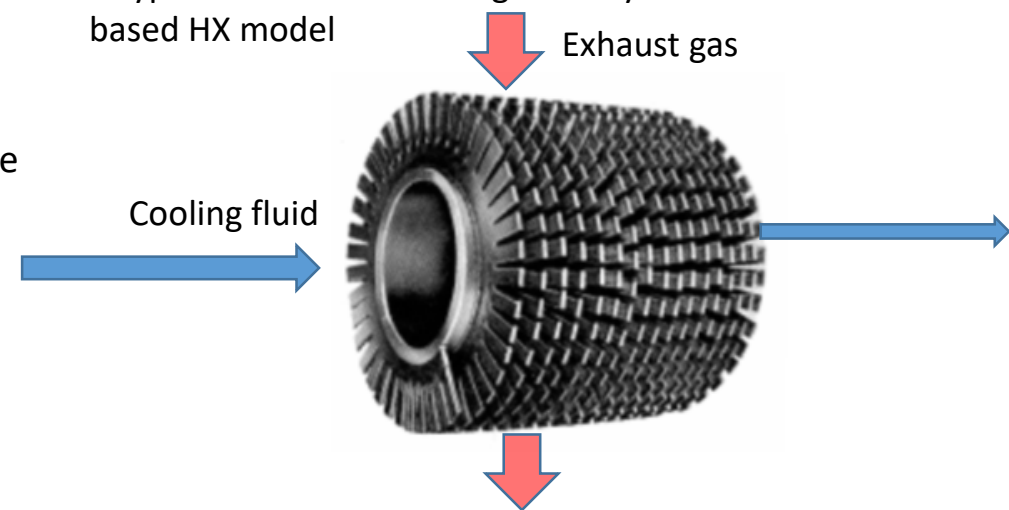


# Different level of detail of heat exchanger models for different tasks

- Pinch-point or UA-based models
  - Estimate power production potential from a given heat source
  - Screening of heat to power technologies for a given application
  - Working fluid screening
- Simplified geometry models
  - Working fluid screening with few candidate working fluids
    - More fair comparison than UA-based models as pressure drop and heat transfer coefficients are based on geometry and fluid properties
  - Initial cycle evaluation of a more detailed study
  - Initial off-design evaluation
    - Especially when HX-type is not determined
- Detailed geometry based models
  - Detailed case studies taking into account heat exchanger type and size
  - Off-design evaluation
  - Component sizing and optimization

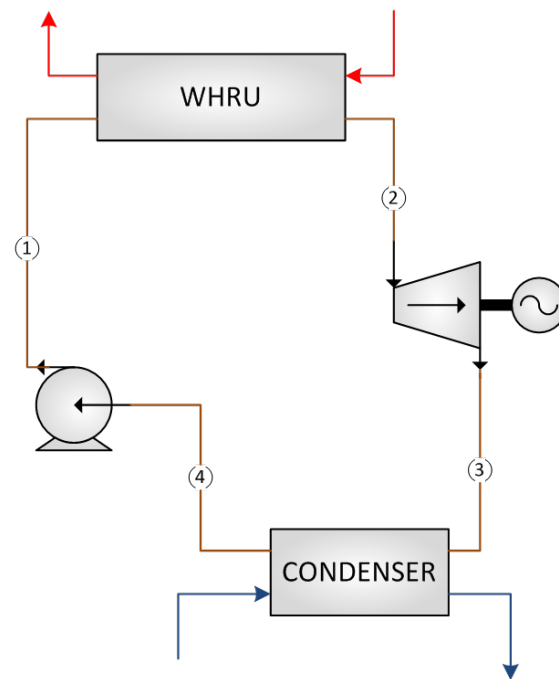
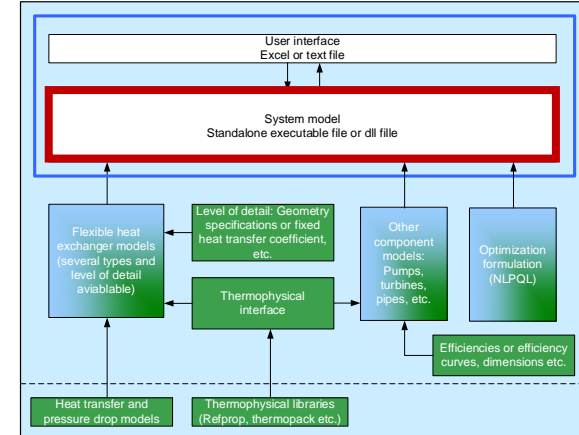


A typical level of detail for geometry based HX model

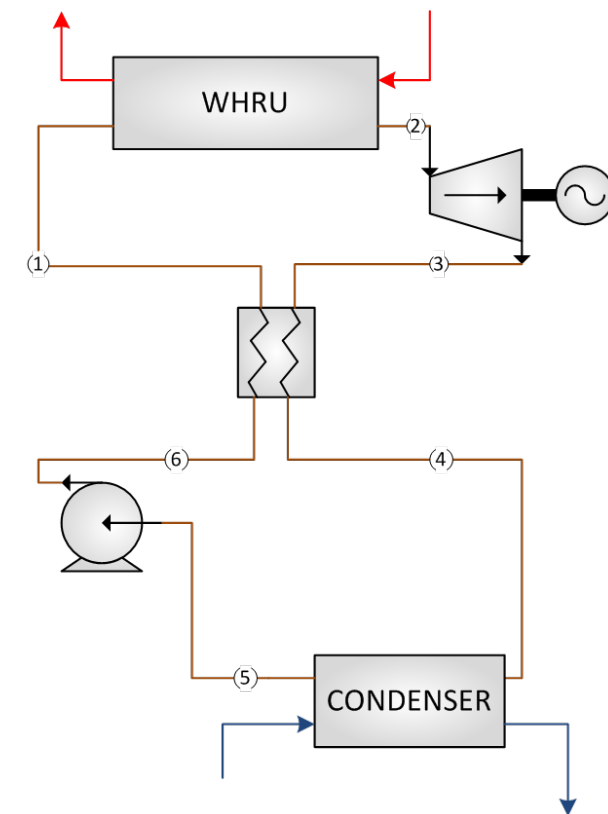


# FlexCS – Available models

- Single stage direct heat recovery systems
  - With or without internal heat recovery
  - Several versions exists in terms of level of details
    - Pinch point analysis
    - UA-based analysis
    - Geometry based FlexHX models
    - Expander efficiency curves

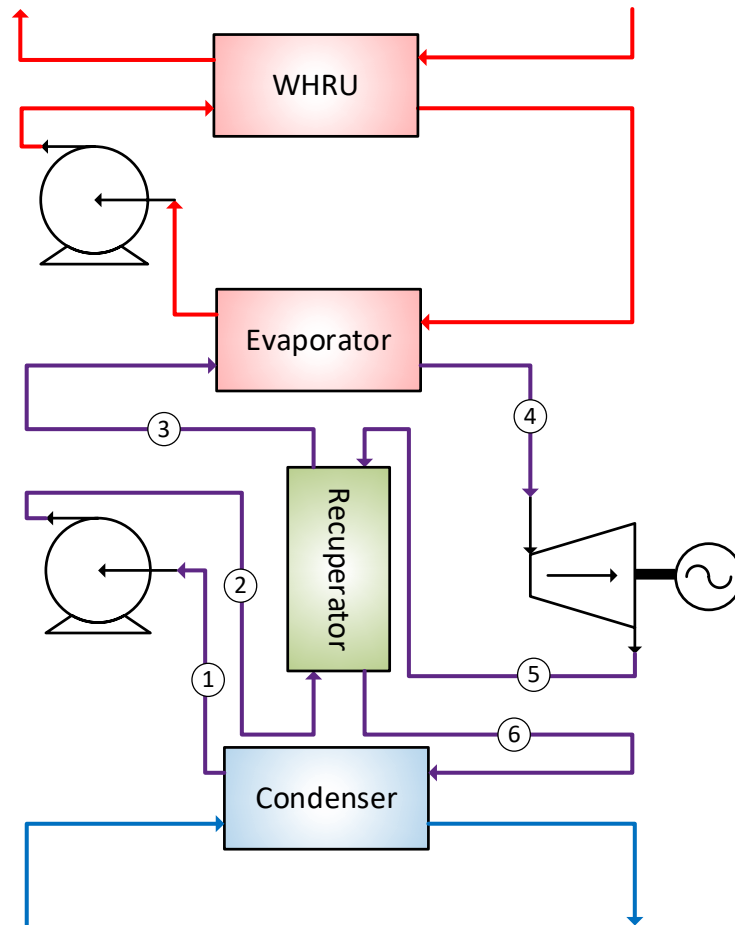
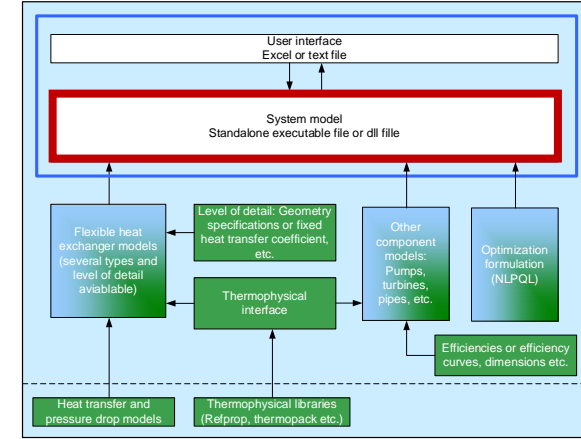


Non-recuperated



Recuperated

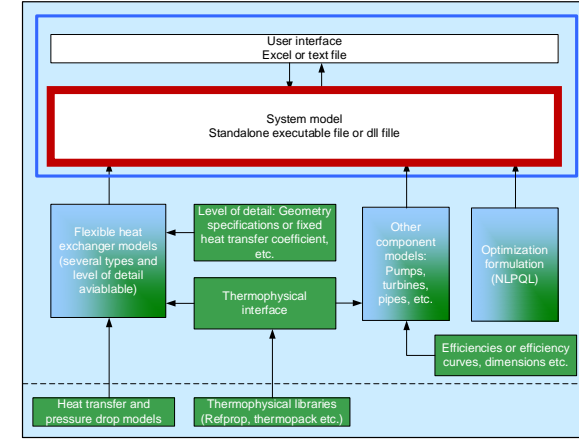
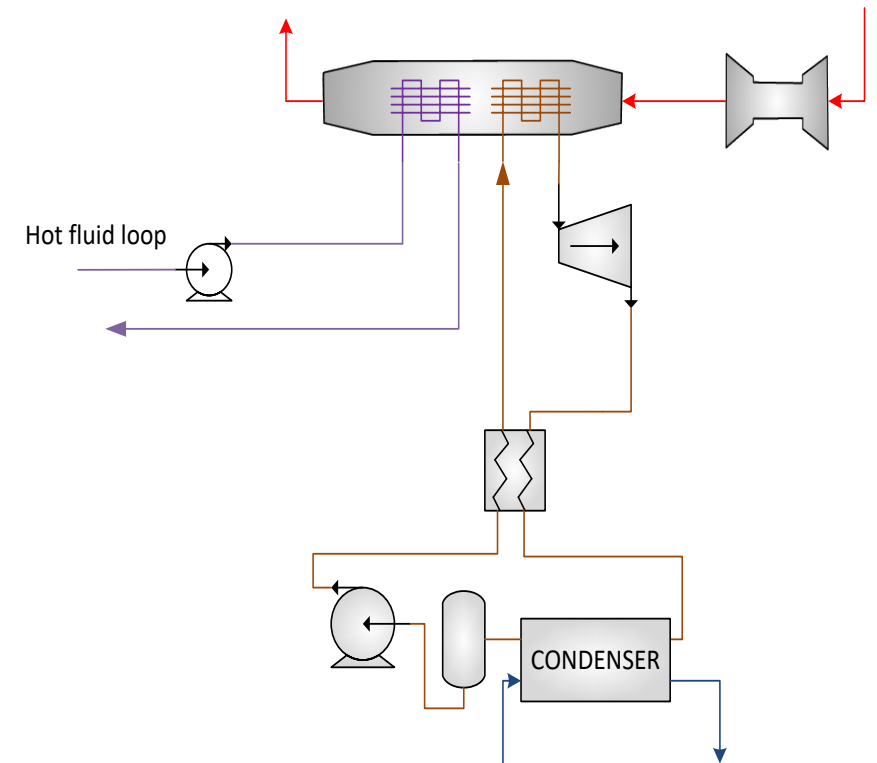
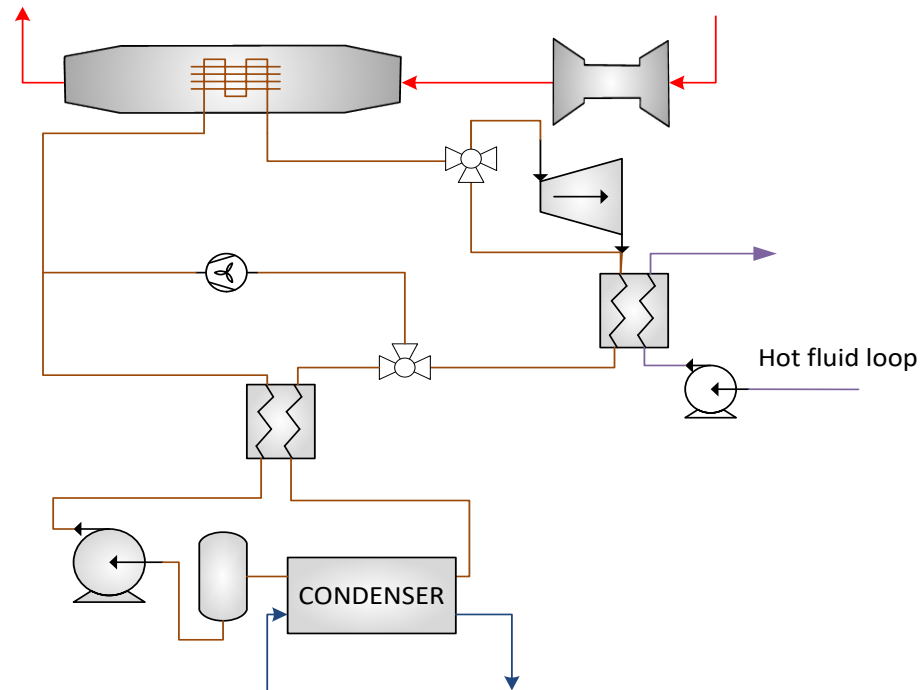
# FlexCS – Available models



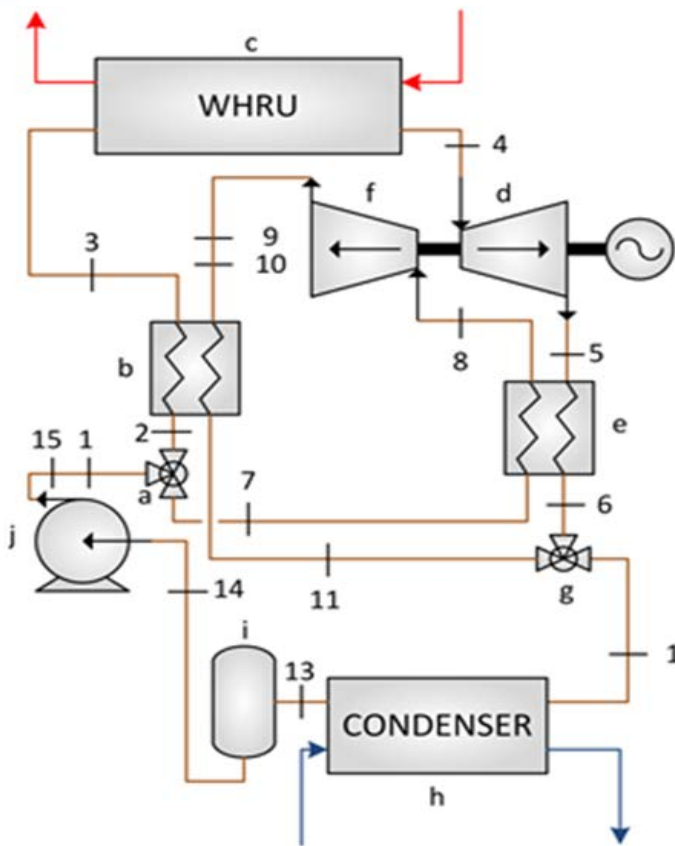
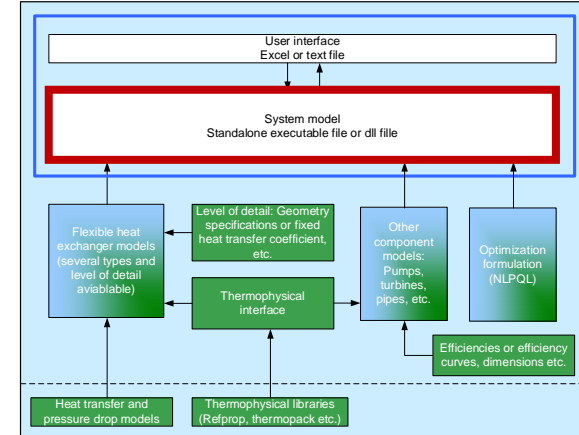
- Single stage indirect heat recovery systems
  - With or without internal heat recovery
  - Developed in HighEFF WP3.1 in 2017
  - Applied by summer researcher Goran Durakovic for analysis of heat recovery from Aluminium industry

# FlexCS – Available models

- Combined heat and power cycle
  - Developed in KPN EFFORT
    - Detailed heat exchanger models from FlexHX or
    - UA-based heat exchanger models



# FlexCS – Available models

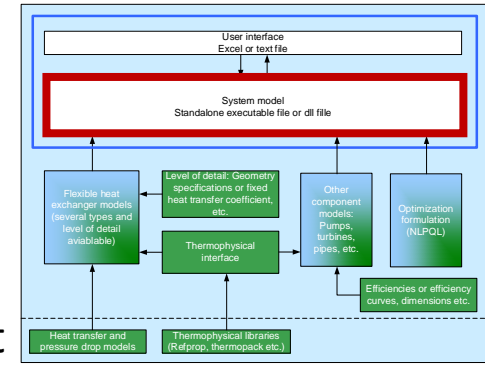


- Dual stage heat recovery systems\*
  - Developed in KPN EFFORT
  - A bottoming cycle model for CO<sub>2</sub> as working fluid
  - Detailed heat exchanger models from FlexHX
  - Also applied in industry projects investigating off-design conditions and part load

\* Walnum H. T., Nekså P., Andresen T. (2013) Modelling and simulation of CO<sub>2</sub> (carbon dioxide) bottoming cycles for offshore oil and gas installations at design and off-design conditions. *Computers and Chemical Energy* 59, 513–520.

# Summary of available models

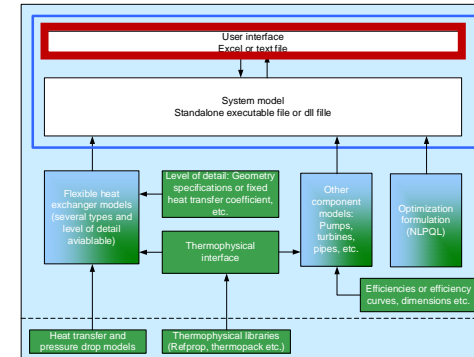
More advanced heat exchanger models towards right



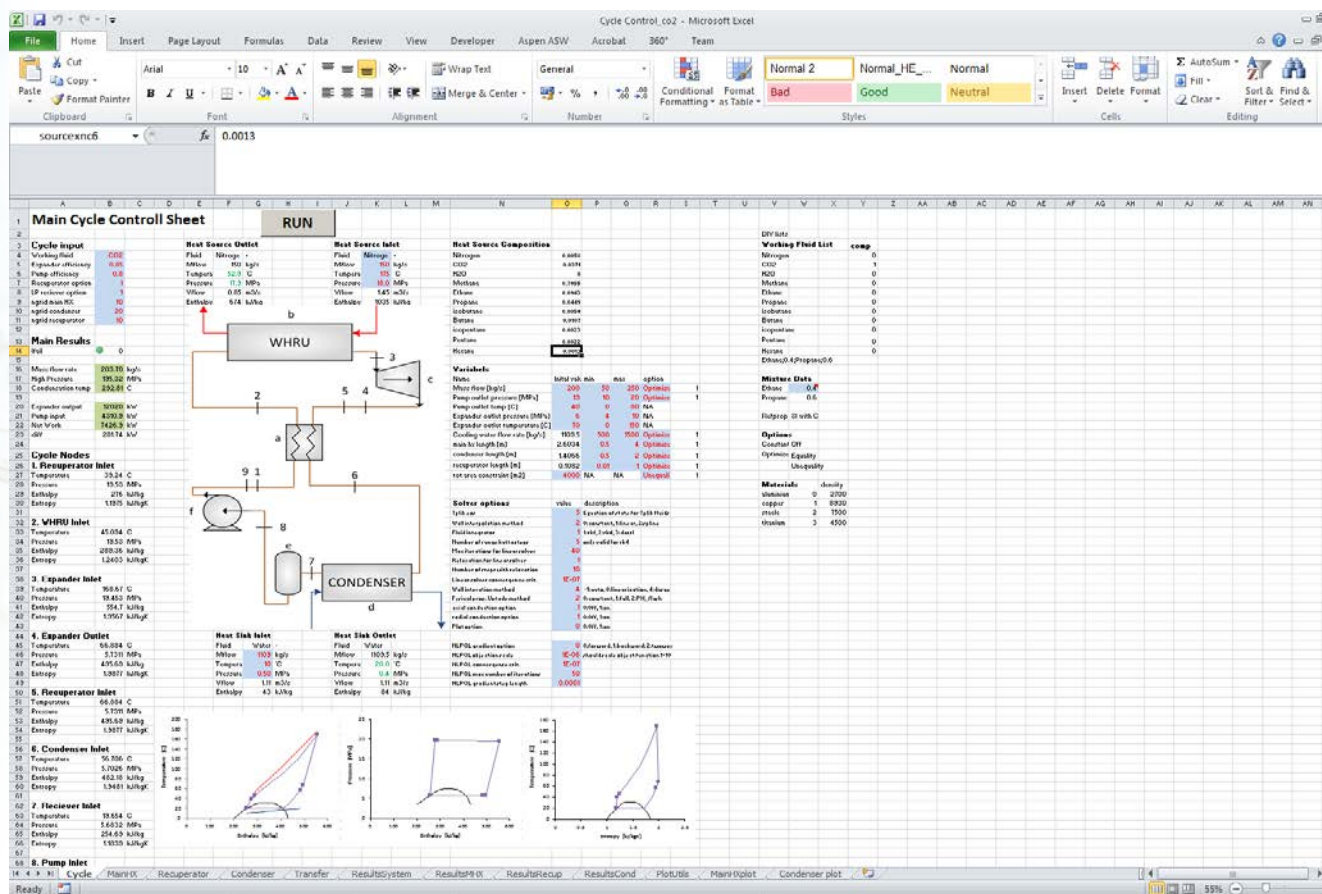
|  | Pinch analysis | UA-based analysis | Simplified geometry | FlexHX HX models                         |
|--|----------------|-------------------|---------------------|--|
| Single stage direct heat recovery      | YES*           | YES*              | YES*                | YES                                      |
| Single stage indirect heat recovery    | YES*           | YES               | NO                  | NO                                       |
| Combined heat and power cycle          | NO             | YES               | NO                  | YES                                      |
| Dual stage/<br>Multiple pressure level | NO             | NO                | NO                  | YES<br>(CO <sub>2</sub> bottoming cycle) |

\* Recently developed

# User interface



## Excel



## Text file

```

# OPTIMIZATION VARIABLES:

#-varmf1_sink -mf1_sink_min:5.0 -mf1_sink_max:20.0 Fixed
-p_wf_highset:55.0E5 # Fixed high pressure if not variable
-varp_wf_high -p_wf_highmin:50.0E5 -p_wf_highmax:60.0E5

-mf1_wf_set:0.8 # Fixed mass flow if not variable
-varmf1_wf -mf1_wf_min:0.5 -mf1_wf_max:3.5

-T_wf_highset:130
-varT_wf_high -T_wf_highmin:100 -T_wf_highmax:150

# Define low pressure directly or indirectly by condensation temperature
#-p_wf_lowset:10e5
#-varp_wf_low -p_wf_lowmin:3e5 -p_wf_lowmax:14e5

-T_wf_condset:23.5
-varT_wf_cond -T_wf_condmin:13 -T_wf_condmax:40

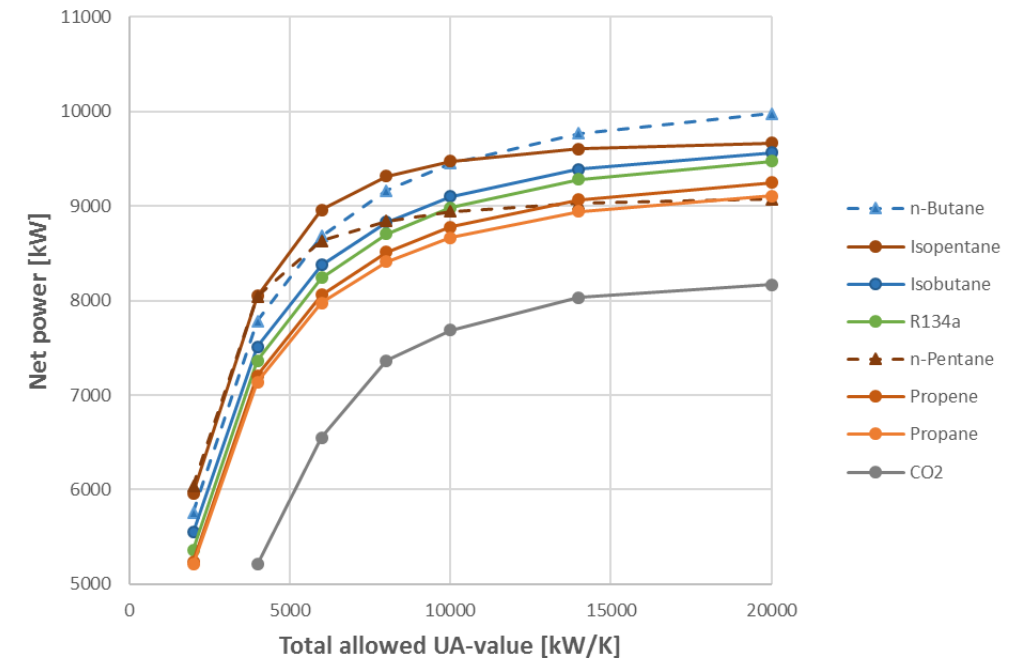
# CONSTRAINTS
-evap_min_DT:2
-cond_min_DT:2
-minSourceTemperature:80
-max_total_A_simple_hx:51.2927
#-fixed_subcooling:0
-expInletSuperheat:
-expOutletSuperheat:

##### NLPQL (solver) parameters
-nlmaxit:30
-nlobjscale:1.0E-4 # Scale factor for objective function
-nlgradopt:2 # Method for numerical differentiation. 0: Forward, 1: Backward, 2: central differentiation
-nleps:1E-6 # Sum of constraint violation ~ sqrt(nleps)
  
```

# FlexCS – Recent development

- Developed simplified power cycle models for screening purposes
  - Single stage cycle with pinch point or UA-based HX models
  - Development of a simplified geometry based HX model
    - Tested in the single stage cycle model
  - These models will be applied next year in HIGHEFF WP2.1 for evaluating the most promising heat to power technologies described and discussed in 2017 activities
- Power cycle models of more realistic layout
  - Indirect heat recovery system model
- Fundamental development
  - Added new correlations for heat transfer and pressure drop relevant for natural working fluid mixture

Example of a UA-based analysis for working fluid screening.  
 Similar analysis can be performed for different heat to power technologies





# FlexCS – Future work

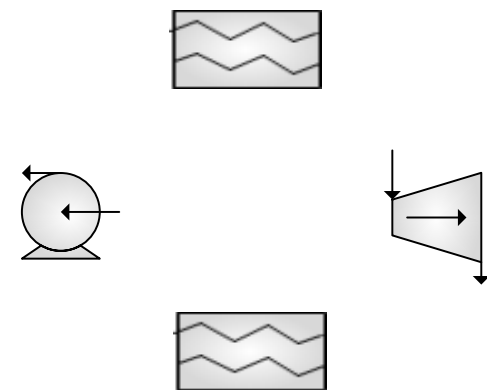
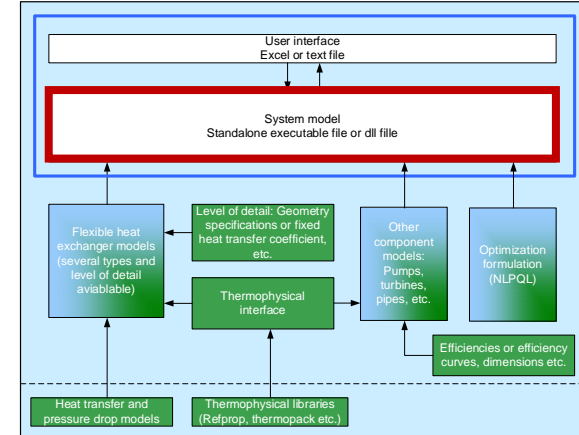
- Develop simplified models of other heat to power technologies
  - Dual stage/dual pressure systems
  - Absorption cycles (Kalina Cycle for instance)
  - Can be used for a quantitative comparison between heat to power technologies
- Further work on simplified geometry heat exchanger models
  - Currently under development
- Expander model
  - Further development of 1D radial turbine model
  - Addition of efficiency curves for scroll and screw expander
- Develop heat pump models
  - Different technology, but applies similar components

## Additional technical slides

- The following slides describe the structure in how to build and solve a system model

# Building and solving system model – The API

- Add components
  - Describing geometry and performance parameters

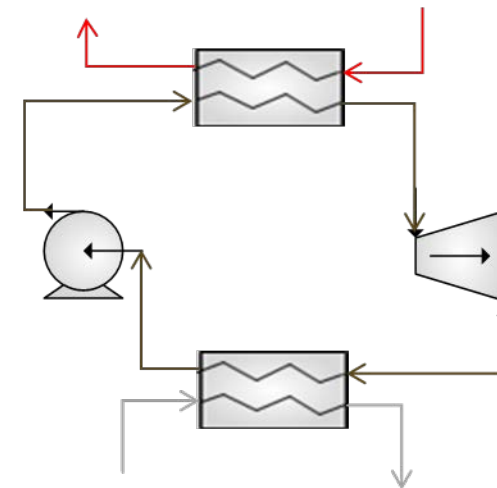
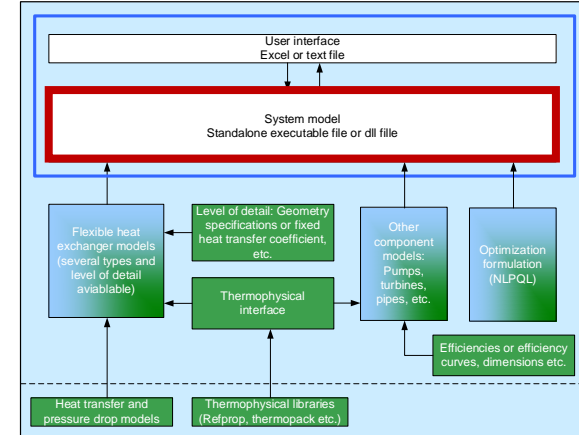


```

FCShx_createFixedUA("evaporator");
FCSSystem_registerHx(system,evaporator);
FCSExpander_createlsentropic("expander", expInlet, expOutlet, eta, nstages)
FCSSystem_registerExpander(system, exp);
...
  
```

# Building and solving system model – The API

- Add components
  - Describing geometry and performance parameters
- Add the streams
  - Contains fluid properties ( $p$ ,  $h$ ,  $\dot{m}$ )
  - Connects the components

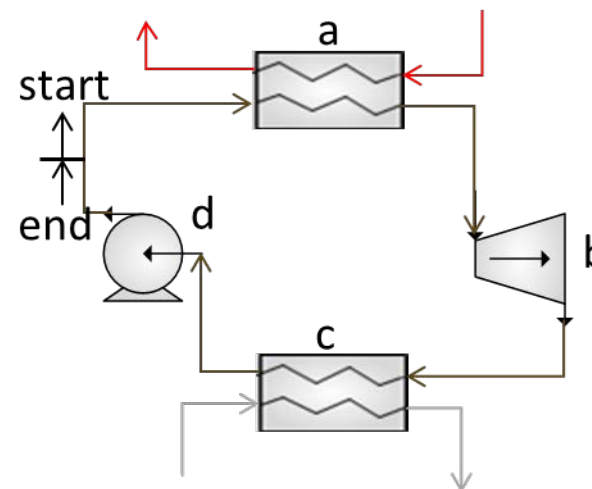
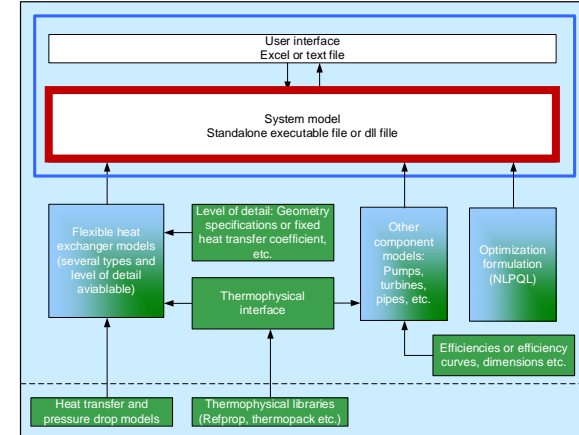


```

evaporatorInlet = FCSSstream_create ("evaporatorInlet", wfcompN->buf,
                                     wflibrary, ncompwf, calctransport, mflRef);
FCSSstream_setMixture (evaporatorInlet, zREF, PRefHigh, TRefHigh);
FCSSstream_setPT (evaporatorInlet, PRefHigh, TRefHigh);
FCSSystem_appendStream (system, evaporatorInlet);
...
  
```

# Building and solving system model – The API

- Add components
  - Describing geometry and performance parameters
- Add the streams
  - Contains fluid properties ( $p$ ,  $h$ ,  $\dot{m}$ )
  - Connects the components
- Set calculation sequence
  - Define starting point



```

FCSHx_solveHx(evaporator, savedata);
FCSExpander_CalculateExpander (expander);
FCSHx_solveHx(condenser, savedata);
FCSCompressor_CalculateCompressor (compressor)
...

```

# Building and solving system model – The API

- Add components
  - Describing geometry and performance parameters
- Add the streams
  - Contains fluid properties ( $p$ ,  $h$ ,  $\dot{m}$ )
  - Connects the components
- Set calculation sequence
  - Define starting point
- Set solver parameters
  - Iteration streams
  - Variables
  - Equality and inequality constraints
  - Objective function

